

**Computational Fluid Dynamics Using Finite Volume Method**  
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**Lecture - 37**  
**Finite Volume Method for Fluid Flow**  
**Calculations: SIMPLE algorithm – Part II**

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6.4)  $C|u|u + \frac{dp}{dx} = 0$   
x-mom. eq.  
continuity eq.  $\frac{d(UA)}{dx} = 0$

1D flow through a porous material

$x_2 - x_1 = x_3 - x_2 = 2$

Use SIMPLE algorithm and calculate  $p_2, U_B$  and  $U_C$

Given:  $C_B = 0.25$   $C_C = 0.2$   $A_B = 5$   $A_C = 4$

$p_1 = 200$   $p_3 = 38$

Initial guess:  $U_B^* = U_C^* = 15$   $p_2^* = 120$

Hello everyone, welcome to another lecture as part of our ME 6151 Computational Heat and Fluid Flow course, ok. So, in the last lecture, we looked at overall simple algorithm on a staggered mesh and we also considered the effect of under relaxation for pressure and the momentum equations.

And finally, we looked at the velocity and the pressure boundary conditions when solving any problem using simple, right. So, in today's lecture, we are going to solve essentially formulate three problems from Patankar's book in chapter 6, that is the fluid flow equation.

So, we look at the each of these problems and formulate them using simple algorithm. So, the first problem we will look at is the problem 6.4 that is shown here; basically this is a 1 dimensional flow through a porous medium and the black circles here indicate essentially locations where the pressure is stored and the red arrows here in the x direction denote the A, B, C denote the staggered locations of the velocity vectors denoted by A, B, C, alright.

I have kind of also shown the corresponding control volumes; of course these extends in the y direction do not make sense, because this is a 1 D problem, ok. So, essentially the area vectors are all 1, ok. But you can see that, there is one control volume; this is basically for control volume for B and this a dashed line this will be control volume for C and this black one this is slightly taller is basically the one control volume for cell 2, that is the primary control volume for the pressure cell, ok.

So, the governing equations are given as  $C|u|u + \frac{\partial P}{\partial x} = 0$  and  $\frac{d(uA)}{dx} = 0$ , ok. So, essentially this equation is basically your, what equation is this? This is your continuity equation, ok. And, what about this guy? This is the momentum or the x momentum equation, ok.

So, alright; now what about, this is the pressure gradient term, area is the cross sectional area that is basically given at what will be the effective area at different location. So,  $A_B$  is 5 units,  $A_C$  is 4 units and also where C is basically the porosity constant that is basically given  $C_B$  equals 0.25,  $C_C$  equals 0.2,  $P_1$  and  $P_3$  are given.

So, basically these two pressures; that means we are given a pressure boundary condition;  $P_1$  is 200,  $P_3$  is 38 that is given. And we were also asked to take initial guess as for the velocities as  $u_B$  star,  $u_C$  star as 15 and the pressure for the cell 2 as 120, ok.

So, essentially this is given and then you are asked to calculate use simple algorithm and calculate what is the final pressure  $P_2$  and the velocities  $u_B$  and  $u_C$ , ok. The grid values that is basically the  $\Delta x$  between 2 and 1 is equals 2. And so,  $\Delta x$  for 2, 3 cell is also equal to 2, ok. So, basically this is a uniform, this is basically uniform mesh, alright.

So, what about the momentum equation? So, this is the pressure gradient term; what kind of a term do you call this guy as  $C|u|u$ ? What kind of a term would this be? This would be would this be convection would this be a convection term? No, it is not a convection term; because if this is a convection term, it is not just that you should have u u, you should also have a nabla operator, right.

You should have some del dot operating on this thing which is not available. So, this is not a convection, is this is of course, not a unsteady term. This is also, is this a diffusion term? No, this is not a diffusion term; there is no nabla operator here. Then what kind of a term this would be? This would be essentially your, the only thing remaining is your source term. So, this would be a source term, ok

And is it linear or non-linear the source term? Source term is non-linear, because you have  $\rho u$  times  $u$ . So, this is a non-linear term, ok. So, you will see how to categorize this particular thing in the formulation, ok. Then let us get started. So, if you remember the, you remember the simple algorithm; what we do is basically write the momentum equations for the velocity control volume.

So, that means, you have to discretize at the momentum equation that is basically this guy at B and at C. Then we essentially write an equation for velocity corrections in terms of pressure corrections from these momentum equations for these staggered control volumes B and C. Then we write the continuity equation, that is for cell 2; that is for the primary cell or for the main cell right, the pressure cell.

Then using the continuity equation, we substitute for the flow rates from in terms of the flow stars and the flow primes. And then we substitute for the flow primes; and the velocity primes in terms of the pressure primes right and then there are a pressure correction equation.

Then we solve for the pressure correction equation and eventually correct the velocities and pressures and kind of keep iterating until the obtained value satisfy both the continuity and the momentum equations, alright.

Then let us get started with discretizing the momentum equation on the cells B and C, ok. And thereafter we will look at discretizing the continuity equation on cell 2, fine. So, the momentum equation is basically  $C|u|u + \frac{\partial P}{\partial x} = 0$ .

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Initial guess:  $u_B = u_C = 15$     $p_2 = 120$

Discretize the momentum equations:  $C|u|u + \frac{dP}{dx} = 0$

Cell - B;   east face: 2   west face: 1

$$\int_1^2 C|u|u \, dx + \int_1^2 \frac{dP}{dx} \, dx = 0$$

? Source term   *Pressure gradient*  
 $S_c + S_p \phi_p$

$S_p = C|u|$ ;    $u_p = u_B$ ;    $S_c = 0$

$$C_B |u_B| u_B (x_2 - x_1) + (p_2 - p_1) = 0$$

So, if we discretize on cell B, cell B has faces as cell B has faces 1 and 2 ok; that means the integration has to go from 1 to 2. We have  $C|u|u$  plus integral 1 to 2  $\frac{\partial P}{\partial x}$  equal 0;  $\frac{\partial P}{\partial x}$  equal 0, this is basically integration on the finite volume. So, we know that this is a pressure gradient term and we just categorize this as a, this as a source term, right. And we know that we can write the source as  $S_c + S_p \phi_p$ .

So, if you consider  $u$  as  $u_p$  means  $u_2$ ; then this is basically comes as your  $S_p$  right, basically  $S_c$  equal 0 and  $S_p$  equal  $C|u|$ , right. And  $S_p$  of course, also needs to be evaluated at the cell centroid. So, the cell centroid for this particular 1 to 2 is basically 2 is basically B right; essentially everything has to be evaluated B and  $u_p$  would be equal to  $u_B$  right, and  $S_c$  equal to 0, alright.

So, we know that this is basically a source term. Then if you write this in terms of the  $S_p \phi_p$  and then  $S_p \phi_p$ ,  $\phi_p$  would be evaluate the cell centroid and that would be a constant. So, constant times integral  $dx$  would give you  $x$  and you have  $x_2$  minus  $x_1$ .

So, that means, essentially what you have is  $C_B \text{ mod } u_B u_B$  times  $x_2$  minus  $x_1$  right that is what we have; that is basically integration of this particular first term. And the second term would be  $dP/dx$ ,  $dx$  integration would be  $dP$  right, integration of  $dP$  would be  $P$ , that would be minus  $P_2$  minus  $P_1$  is what you get here, ok.

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Source term  
 $S_c + S_p \phi_p$

Pressure gradient

$S_p = C|u|$ ;  $u_p = u_B$ ;  $S_c = 0$

$C_B |u_B| u_B (x_2 - x_1) + (P_2 - P_1) = 0$

$C_B |u_B| \Delta x u_B + (P_2 - P_1) = 0$  discrete mom. eqn. for cell B

$a_B u_B = (P_1 - P_2)$  — (1)

Compare  $a_e u_e = \sum a_{nb} u_{nb} + \Delta y (P_p - P_e) + b_e$

So, for cell B, now we pretty much have the discrete momentum equation; that means  $C_B \text{ mod } u_B u_B \text{ times } x_2 - x_1$ . So, if I write whatever is being multiplied with  $u_B$ , that is  $C_B \text{ mod } u_B \Delta x$  as a coefficient  $a_B$ ; then the equation we have is  $a_B$  times  $u_B$  plus  $P_2 - P_1$  equal 0, right. That means, this is the; this is the discrete momentum equation for cell B right;  $a_B u_B = P_1 - P_2$ .

Now,  $a_B$  here is the coefficient it is more like your,  $a_p$  term, right. So, if you compare with your original equation; if you remember we wrote  $a_e u_e = \sum a_{nb} u_{nb} + \Delta y (P_p - P_e) + b_e$ , right. So, in this particular case if you compare, you do not have  $b_e$ ; you do not have contribution coming from  $\sum a_{nb}$  here, because otherwise you should have got a term which is like  $u_c$  times something that is not there. So, only the central coefficient that is  $a_e u_e$  is basically  $a_B u_B$ .

Now,  $a_B$  is basically the coefficient for  $u_B$ , alright. So, that is the discrete equation for cell B. Now, if you move on we will do a similar thing; integration of the momentum equation for cell C, that is basically for this cell centroid. So, the limits of integration would be for faces that is 2 to 3.

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Cell - c : east-face : 3 ; west-face : 2

$$\int_2^3 c|u|u dx + \int_2^3 \frac{dp}{dx} dx = 0$$

$$c_c |u_c| \Delta x u_c + (p_3 - p_2) = 0$$

$\underbrace{c_c |u_c| \Delta x}_{a_c}$ 
↑ discrete mom. eqn. for cell C

$a_c u_c = (p_2 - p_3)$ 
cell - c
②

Starred-momentum equations:  $a_B u_B^* = (p_1^* - p_2^*)$  — ③

$a_c u_c^* = (p_2^* - p_3^*)$  — ④

And then integrate in a similar way and up time essentially for cell 3 we have west face is 2, east face is 3. So, we have to go from 2 to 3  $C \text{ mod } u \text{ d } x$  plus integral 2 to 3  $\frac{\partial P}{\partial x}$ . Then again this is basically your  $S_c + S_p \phi_p$ . So, this would come out to be  $C_c \text{ mod } u_c \Delta x$  times  $u_c$  plus  $\frac{\partial P}{\partial x}$  integration would be pressure; that means we will apply the limits we have  $P_3$  minus  $P_2$  and equal 0, ok.

And this coefficient whatever is multiplying  $u_c$ , if we take it as a constant; that is the basically the coefficient, because we have to linearize the system right, this is what is the linearized source term. And  $S_p$  is known while we are doing the inner calculations, right. So, that is why  $C_c \text{ mod } u_c \Delta x$  would be the constant if we call it as  $a_c$ . What we have is basically  $a_c u_c$  equals  $P_3$  minus  $P_2$ . So, this is the discrete momentum equation for cell C, ok. So, we have the both the momentum equations.

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Star-momentum equations:  $a_B u_B^* = (p_1^* - p_2^*)$  — (3)  
 $a_C u_C^* = (p_2^* - p_3^*)$  — (4)

Eqn (1) - (3):  $a_B u_B' = (p_1' - p_2')$   
 Eqn (2) - (4):  $a_C u_C' = (p_2' - p_3')$  } Prime eqns. SIMPLE approx.

But given  $p_1 = 200$  &  $p_3 = 38$ ;  $\therefore p_1' = 0$  &  $p_3' = 0$

$\Rightarrow a_B u_B' = -p_2'$ ;  $a_C u_C' = p_2'$   
 $u_B' = -p_2'/a_B$ ;  $u_C' = p_2'/a_C$

So, if you were to write in terms of the star quantity. So, essentially we just have to apply for a given pressure guess and a velocity guess; what would be your velocities that you converge to? So, in this particular case, we do not have a system to solve; because what we have is  $u_B^*$  expressed as pressure star. So, the moment you have a guess value for pressure, you can calculate what is the value for converged value for  $u_B^*$ , alright.

So, that means, your start momentum equations are  $a_B u_B^* = P_1^* - P_2^*$ ; that is basically let us call it as equation 3. Then  $a_C u_C^* = P_2^* - P_3^*$ , ok. So, this is basically the star momentum equation for the cell C, ok. Now, what do we have to do?

We have to subtract the star momentum equations from the original equation right; that means we take equation 1 and subtract equation 3, similarly we take equation 2 and subtract equation 4. That means, what we get is, we get  $a_B u_B$  minus  $a_B u_B^*$  which will basically give you  $a_B$  times  $u_B$  minus  $u_B^*$  that is basically your  $u_B'$ .

So, equation we get is  $a_B u_B'$  equals; similarly on the right hand side the non star values and the star values subtract of leading to the prime values that will be  $P_1' - P_2'$ . And similarly we have another equation that is  $a_C u_C'$  equals  $P_2' - P_3'$ , ok. So, these are the, these are the velocity corrections expressed in terms of pressure corrections.

Now, what you see here is that, this is we do not have to apply the simple approximation here right, which was neglecting the contribution of  $a_{nb} u_{nb}'$  primes and  $u_{nb}'$  here;  $a_{nb} u_{nb}'$ ,

because those are already 0 here. So, as a result, the simple algorithm need not be, the simple algorithm approximation need not be directly applied here; because the equations that we obtained already satisfy this condition that, the neighboring contribution is already 0 to the velocity corrections, alright.

But we were given what is the pressure at the locations 1 and 3. So,  $P_1$  equals 200 and  $P_3$  equals 38 this is what is already given; that means because the pressure is given, what will be the pressure corrections at these locations? They should be 0 that is why; that means  $P'_1$  equal 0 and  $P'_3$  equals 0, alright.

So, those are 0, that means if you substitute here;  $P'_1$  is 0 and  $P'_3$  is 0. So, the equation we get is  $a_B u'_B$  equals  $-P'_2$ ; then we can write  $u'_B$  as  $-P'_2/a_B$ . Similarly,  $a_C u'_C$  equals  $P'_2$  right; because  $-P'_3$  is 0, then  $u'_C$  equals  $P'_2/a_C$ , ok.

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velocity corrections  
in terms of  
pressure corrections

$$u'_B = -P'_2/a_B; \quad u'_C = P'_2/a_C$$

Discretize continuity equation: on cell for pressure: cell-2

cell-2; east-face: C; west-face: B

$$\int_B^C \frac{d}{dx} (uA) dx = 0.$$

discrete continuity  
equ. for cell-2

$$u'_C A_C - u'_B A_B = 0.$$

$$(u'_C + u'_C) A_C - (u'_B + u'_B) A_B = 0$$

$$u'_C A_C - u'_B A_B = u'_B A_B - u'_C A_C$$

So, these are basically your velocity corrections in terms of pressure corrections, right. Essentially we just have only three cells, two velocity cells B and C and one pressure cell that is  $P_2$ . We just have to calculate what is the converged values for  $u_B$ ,  $u_C$  and  $P_2$ , alright. Now, we are done with essentially discretizing the momentum equations. So, we will go and look at discretizing the continuity equation on the primary cell, on the cell for pressure that is basically cell 2, ok.



So, if you look at cell 2, the faces that we have are B is there on the left hand side and C is there on the right hand side; so that means if we go back. So, we have for pressure cell 2, that is this black cell we have the faces are B to C, ok. So, essentially we will integrate the continuity equation for B to C and the continuity equation is given as  $\frac{d(uA)}{dx} = 0$ .

So, that is what is given, that means if you integrate this you are going to get  $uA$  and if you substitute the face values what we get is,  $u_C A_C$  minus  $u_B A_B$  equal 0. So, this is your discrete continuity equation for pressure cell 2, alright. Now, we know that of course, because these are the corrected values as such  $u_B$  and  $u_C$  that if we represent them, then these are equal to 0; but if these were starred values  $u_C^*$  and  $u_B^*$ , they would not satisfy the continuity equation, right.

As a result we can of course, now decompose this  $u_C$  into star and prime, similarly  $u_B$  into star and prime; then what you get is  $u_C^*$  plus  $u_C'$  times  $A_C$  minus  $u_C^*$  plus  $u_B'$  times  $A_B$  equal 0, right. So, that means, we have decomposed this into star and prime values; then we can send the star values to the right hand side, because those are known at this particular time, right.

Essentially we can send  $u_B^*$  and  $u_C^*$  times  $A_C$  and  $u_B^*$  times  $A_B$  to the right hand side. So, what you get is, you get minus  $u_B^* A_B$  going to the right hand side makes it  $u_B^* A_B$  and you have plus  $u_C^* A_C$  become minus  $u_C^* A_C$  on the right hand side.

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known after the mom. eqns. are converged.

velocity corrections in terms of pressure corrections...

$$u_C' A_C - u_B' A_B = u_B^* A_B - u_C^* A_C$$

But  $u_C' = p_2' / a_C$ ;  $u_B' = -p_2' / a_B$  substitute

$$p_2' \left( \frac{A_C}{a_C} \right) + p_2' \left( \frac{A_B}{a_B} \right) = u_B^* A_B - u_C^* A_C$$

Pressure Correction Equation

$$p_2' = \frac{(u_B^* A_B - u_C^* A_C)}{\left( \frac{A_C}{a_C} + \frac{A_B}{a_B} \right)}$$

So, this is basically what is already known after the momentum equations are converged, right alright. That means, what we have left with this, you have you are left with  $u'_C A_C$  minus  $u'_B A_B$  equals such and such on the right hand side. Now, why do we do essentially?

We substitute for the velocity corrections right; we substitute for the velocity corrections in terms of pressure corrections right from the equations we have derived. So, that means, substitute for  $u'_C$  in terms of pressure correction that is basically  $u'_C$  equals  $P'_2 A_C$ ; similarly  $u'_B$  equals  $-P'_2 A_B$ .

So, substitute for these two; that means plug in these two into this equation. So, what we get is  $P'_2$  times  $A_C/a_C$ . So, capital  $A_C$  is the cross sectional area that is given, little  $a_C$  is the coefficient of  $u_C$  right in the momentum equation. Similarly, you get a  $u'_B$  has got a minus,  $u'_B$  has got a  $-P'_2/A_B$ , as a result this becomes plus.

So, what you get is  $P'_2$  times  $A_B/a_B$  equals, on the right hand side as usual we have  $u_B^* A_B$  minus  $u_C^* A_C$ . So, essentially we got an equation here; this is basically  $P'_2$  times  $A_C/a_C$  plus  $A_B/a_B$  equals  $u_B^* A_B$  minus  $u_C^* A_C$ , ok.

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Pressure Correction Equation

$$P'_2 = \frac{(u_B^* A_B - u_C^* A_C)}{\left(\frac{A_C}{a_C} + \frac{A_B}{a_B}\right)}$$

one cell;

Correct velocity and pressure

$$u_B = u_B^* + u_B' = u_B^* - \frac{P'_2}{a_B}$$

$$u_C = u_C^* + u_C' = u_C^* + \frac{P'_2}{a_C}$$

$$P_2 = P_2^* + P_2'$$

Because of non-linearity in the source term; under-relax

So, we can rewrite this, basically this is now your pressure correction equation in terms of the right hand side B right the star values and the coefficients, ok. So, this is your pressure correction equation. Now, in this particular case, because we have only one cell; we do not

have to solve a Gauss Seidel, right. But in general, this would be similar to  $a_p P_p'$  equals  $\sum a_{nb} P_{nb}' + b$ , ok.

So, you should be able to make these comparisons at any stage. But once we calculate what is the right hand side value here; we can calculate what is  $P_2'$ , that means we will know what is the pressure correction. So, once you know the pressure correction, you can substitute into the velocity corrections, calculate the velocity corrections; then pressure and velocity can be corrected and the algorithm is complete.

You can go back and to the step, you know the previous step where we have guess the velocity and pressure and then flow down from there again, right ok. That means, once you know the pressure correction and velocity correction; you can correct the pressure that is  $P_2$  equals  $P_2^*$  plus  $P_2'$ .

Similarly, velocities are  $u_B = u_B^* + u_B'$ , where  $u_B^*$  is the converged value from the momentum equation and  $u_B'$  equals in terms of pressure corrections that is  $-P_2'/A_B$  and  $u_C = u_C^* + u_C'$  that is  $u_C^*$  plus  $u_C'$  equals  $P_2'/A_C$ , ok.

So, we have we now got  $u_B$ ,  $u_C$  and  $P_2$  these  $u_B$  and  $u_C$  of course, now satisfy continuity equation; but they do not satisfy the original momentum equation, because the momentum equation itself is non-linear, right. We have  $C \text{ mod } u$ , where  $C \text{ mod } u$  itself we was taken as  $u_{A_B}$ ,  $A_B$  contains  $u_B^*$  values right, which are now got updated. So, they do not satisfy the momentum equations, the velocity.

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Under-relax momentum equations:

Cell B:  $a_B u_B^* = (P_1^* - P_2^*)$  previous iteration value; latest value

mom. eqn. when you solve cell B:  $\left(\frac{a_B}{\alpha_u}\right) u_B^* = (P_1^* - P_2^*) + \left(\frac{1 - \alpha_u}{\alpha_u}\right) a_B u_B^{**}$

Cell C:  $a_C u_C^* = (P_2^* - P_3^*)$  current iteration value..

$\left(\frac{a_C}{\alpha_u}\right) u_C^* = (P_2^* - P_3^*) + \left(\frac{1 - \alpha_u}{\alpha_u}\right) a_C u_C^{**}$

So, because of the non-linearity of course, they do not satisfy. And we also have to under relax the equations, because of the nonlinearity in the source term, ok. So, let us under relax the pressure; that means whatever is the  $P_2'$ , you got you only obtain multiply that with some alpha p and add it to the star value to obtain the original value.

So,  $P_2 = P_2^* + \alpha_p P_2'$ . And of course, we know that we will not. So, basically do not under relax velocity in this way right; because if you do it this way, because then it will not satisfy the continuity equation. So, we go back and use the, in the context of momentum equations itself whenever we are trying to solve it; we have to under relax and use the under relaxed equations.

That means, our original equation for cell B is  $a_B u_B^* = P_1^* - P_2^*$ . So, if you under relax this equation, basically this is your  $a_p$ ,  $a_p$  value right; this is like  $a_B \phi_p$  right.

That means, you get  $a_B/\alpha_u$  times  $u_B^*$  equals  $P_1^* - P_2^*$  plus; for this contribution you would have  $(1 - \alpha_u)/\alpha_u$  times  $a_B u_B^*$ . I have  $u^*$  star here, basically to indicate that this is the previous iteration value or the latest value that we have, that is that we can use here.

And essentially to make sure that this is different from what we have here, ok. So, you would use this momentum equation when you solve for the cell B ok; because this is the under relaxed equation and you can take some value for  $\alpha_u$  as 0.8 or something.

And this under relaxation is necessary, because of the non-linearity in the source term, ok. That means you will use this equation instead of the equation we have written here in and you try to solve. So, when you try to solve the star momentum equations instead of 3 and 4, you would use the under relaxed equation.

Now, that means, if you look at cell C; what we have is  $a_C u_C^*$  equals  $P_2^* - P_3^*$ . If you also under relax this equation with the same factor  $\alpha_u$ , what you get is  $a_C/\alpha_u$  times  $u_C^*$  right equals  $P_2^* - P_3^*$  plus on the right hand side you have to add this extra term that is  $(1 - \alpha_u)/\alpha_u$  times  $a_C u_C^*$  star, this also has to be essentially star, right.

Basically I forget to write it here, this is also star star; indicating that this is the current iteration value that is available right, that is available, excuse me, right ok. So, essentially you would use these two equations in the solution of the star momentum equations. So, when you after you have guess the pressure and we guess the velocities, you would use this equation to solve for convergence of these values to solve using the Gauss Seidel or something.

In this particular case you do not have to; because you know all these things on the right hand side, so it can be computed, ok. Of course, now because we have modified the this above equation to use under relaxation; we not only need pressure guess, but we also need the velocity guess in order to calculate the velocity values, alright.

So, now the algorithm is actually complete; we have to of course write a code for this and run it, so that we would obtain the values for  $u_B$ ,  $u_C$  and  $P_2$ , ok. So, that we will do it in the next class; but for today we will do the remaining two problems as well and formulate them as such.

Now, one question you may have is ok, what about. So, instead of using this equation, now what we are saying is that we will use this equation with under relaxation. But do not we have to go back and re do everything; because if we have change the momentum equation, do not I have to go back and do the these correction equations again.

You are right for example, now that. So, instead of 3 and 4 we are going to use the corresponding under relaxed equations; then do not I have to redo all these calculations of  $u'_B$  and use the correct equations, is not it the under relaxed equations or not? So, that is the question.

The question is, why am I doing 3 4? Why are we obtaining these from this equation and then we are saying ok, we cannot solve this equation; we want to do under relaxation and change these equations to something else right, which are the corresponding under relaxed equations.

Now, the idea is, even if you use the under relaxed equations here; in the simple approximation you will have those terms also will be neglected, just like the  $\sum a_{nb} u'_{nb}$ , the contribution coming from this  $\sum a_{nb}$ ,  $\sum a_B u'_B$  also will be neglected, ok. So, essentially you will, they will not be considered; that is simple approximation, excuse me.

So, as a result it does not matter whether you had use the under relaxed equation for deriving the velocity correction pressure correction equation or the regular equation, fine. So, that finishes the setting up of the first problem that is the problem 6.4.

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6.5)

Continuity eqn.  $\frac{d}{dx} (\rho u A) = 0$

x-mom. eqn.  $\frac{d}{dx} (\rho u A u) = -A \frac{dp}{dx}$

$\rho = 1$  everywhere;

$A_A = 3; A_B = 1; p_1 = 28; p_3 = 0$

Fluid upstream of point 1 has negligible momentum.

Calculate  $U_A, U_B$  and  $p_2$

Initial Guess:  $U_A^* = 5/3; U_B^* = 5;$   
 $p_2^* = 2.5.$

approximation that is asked to be made

Let us move on to the second problem that is 6.5 from the, from chapter 6 of Patankar's book, ok. So, what this is basically, this is a again a this is a flow through a converging nozzle, ok. And the flow is going in the positive x direction. So, it is going from essentially left to right. So, there is a converging nozzle and then again the values 1, 2, 3 here locations denote the places where the pressure is stored and A and B denote the locations where the velocities are stored, alright.

Then two equations are given, the first one is  $\frac{d(\rho u A)}{dx} = 0$ . What is this equation? This is basically your continuity equation, right. And, what about this guy? This is  $\frac{d(\rho u A u)}{dx} = -A \frac{dP}{dx}$ . what is this equation? This is your x momentum equation. Now, what about the terms here? Of course, this is the pressure gradient. And what is this term? This is now; this is now the convection term right; basically  $\rho u A u$  this is basically the convection term, ok.

So, we have and we do not have any source term. So, source term is 0. Also the effective areas at these locations are given at A and B, ok. And the density can be taken to be 1 everywhere that is what is given; then because this is a nozzle, so beyond 1 the area kind of grows very large, as a result the velocity is quite small here, ok. And the area is very large and the velocity is very small ahead of upstream of 1, ok.

So, the effective areas are given, area cross sectional area at A is 3, cross sectional area at B is 1 and the pressures are given. Again this is similar to the previous problem, with all the boundary conditions given are the pressure  $P_1$  is 28 and  $P_3$  is 0 that is what is given.

And it is also given that fluid upstream of 0.1, basically here has negligible momentum, right. That means upstream of 1 has negligible momentum; that means the flow rate upstream of this can be taken to be 0, because if we denote flow rate as  $\rho u A$ , the momentum is mass times velocity.

So, mass is your  $\rho A$  times  $u$ , right. So, upstream of 1 here velocity is so small and the cross sectional area is so large and essentially the momentum can be taken to be very small, alright. That is this is an approximation that is given, ok. So, this is an approximation that is asked to be made while solving problem, fine.

Then what else essentially you are asked to calculate what is the velocities at a locations A and B, that is the A and B is the velocity control volumes and at the pressure control volume that is  $P_2$ . So, you have to calculate what is  $u_A$ ,  $u_B$  and  $P_2$  and it is basically given that  $u$  is initial guess five thirds for  $u_A$ , 5 for  $u_B$  and 25 for pressure ok.

That is basically when you write the code, you can use this as the initial guess and solve the equations. As of now we will try to set up the complete algorithm using simple, ok. So, again what is the first step? First step is to write the momentum equations for the

velocity control volume that is for A and B, write the momentum equations; then derive the prime equations a star equations and prime equations for A and B.

Then write the continuity equation discretization for cell 2 and relate the velocity corrections that you got from A and B in terms of pressure corrections and substitute for pressure corrections, essentially get a pressure correction equation, right. So, that is the idea.

So, we start off with momentum equation that is this equation discretize for A; then discretize for B, followed by discretize this for cell 2, ok. So, for cell A we have 1 and 2 as the faces, for cell B we have 2 and 3 as the faces, and for cell 2 the pressure cell we have A and B as the faces that is kind of good to remember, alright.

(Refer Slide Time: 29:01)

Cell-A:  $\int_1^2 \frac{d}{dx} (\underbrace{\rho u A}_{F}) dx = \int_1^2 -A \frac{dp}{dx} dx$

Convection term;  
UDS  
Flow is in the positive  
x-direction All  $F > 0$

$F_2 u_2 - F_1 u_1 = -A_A (p_2 - p_1)$

$F_2 > 0 ; u_2 = u_A$   
 $F_1 > 0 ; u_1 = u_{\text{upstream}} ; \text{but } F_1 \approx 0 \text{ (given)}$

$F_2 u_A = A_A (p_1 - p_2)$

Cell-B:  $\int_2^3 \frac{d}{dx} (\rho u A) dx = \int_2^3 -A \frac{dp}{dx} dx$

So, cell A is basically going from 1 to 2. So, what we have is integral 1 to 2  $\frac{d(\rho u A)}{dx} dx$  equals integral 1 to 2 on the right hand side we have  $-A \frac{dp}{dx} dx$ , ok. This being the convection term, we can write this as the flow rate that is basically  $\rho u A$  equals  $F$  times  $u$ . So, if you apply gauss divergence theorem and so on what you basically get is, you get  $F$  east, right. Or you can even integrate it here, because this is 1 D, you do not need to involve gauss divergence theorem.

So, this basically gives you  $\rho u A$  that is  $F$  times  $u$ ; you calculate at both the limits that is  $F_2 u_2 - F_1 u_1$ , right. And on the right hand side, we have minus  $A$ ; because this is a



coefficient this, this is taken to be at the cell centroid value. So, for cell A, this is basically  $A_A$ , this is  $-A_A$  times integral  $\frac{dP}{dx} dx$  would give you integral dP which will give you pressure; that means if you apply the limits this is basically  $P_2 - P_1$ .

Now, of course, because we are given the convection term ok; we will make an approximation, we will use the upwind difference scheme. Although it is not specified in the problem, we will apply upwind difference scheme; we will use upwind difference scheme essentially. What that means is that, if  $F_e$  is greater than or equal to 0, then  $u_e$  equals  $u_P$  or if  $F_e$  is less than 0, then  $u_e$  equals  $u_E$ .

But fortunately in this case, you do not have to look for less than 0 cases; because all the flow rates are positive right, because the flow is going from in the essentially flow is in the positive x direction. As a result all F values are greater than or equal to 0. In fact, all are greater than 0; because there is some flow that is happening.

That means,  $F_2$  is, because  $F_2$  is greater than or equal to 0; what will be the value of  $u_2$ ?  $u_2$  is basically, if you go here  $F_2$  is positive. So,  $u_2$  can be taken to be it is up steam value that is  $u_A$ , right.

Similarly, if  $F_1$  is positive, what will be the value of here? The value here would be  $F_1$  is positive,  $u_1$  can be taken whatever u upstream of 1 right; that means  $F_2$  is because it is positive,  $u_2$  can be taken as the upstream value and  $u_1$  can be taken as u upstream of 1, ok.

But it is given that the momentum up stream of 1 can be can be neglected; that means  $F_1$  can be taken to be 0, as a result this term is 0; that means what we are left with is we are left with  $F_2 u_A$  equals  $-A_A$ . Or I, if I observe the minus inside, we can write this as  $A_A$  times  $P_1 - P_2$ , alright.

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Handwritten notes on a whiteboard:

$$F_2 u_A = A_A (P_1 - P_2)$$

Cell B:  $\int_2^3 \frac{d}{dx} (\rho u A u) dx = \int_2^3 -A \frac{dp}{dx} dx$

$$F_3 u_3 - F_2 u_2 = A_B (P_2 - P_3) \quad \text{UDS for the convection terms}$$

$F_2 > 0; \quad u_2 = u_A$

$F_3 > 0; \quad u_3 = u_{B_3}$

$$F_3 u_B - F_2 u_A = A_B (P_2 - P_3)$$

So, we have  $F_2 u_A$  equals  $A_A$  times  $P_1 - P_2$ . And if we do the same exercise for cell B; what we get is integral 2 to 3, because for cell B we have the faces is 2, 3, right. So, that means, we can write this as integral 2 to 3  $\frac{d(\rho u A u)}{dx} dx$  equals 2 to 3  $-A \frac{dP}{dx} dx$  alright; that means again this is F times u.

So, is the integration value apply that at the both the limits, you get  $F_3 u_3 - F_2 u_2$  equals cross sectional area for cell B is  $A_B$ , that is evaluate the cell centroid times integral  $\frac{dP}{dx} dx$  would give you dP.

So, this is basically pressure, integral dP would be pressure; that means  $P_3 - P_2$ . Or if you observe the minus inside, you get  $A_B$  times  $P_2 - P_3$ , that is understood. Now, of course, you have to apply again upwind difference scheme for the convection terms right; that means  $F_3$  because  $F_2$  is positive, so  $u_2$  equals  $u_A$  and  $u_3$  equals  $u_B$ , right.

So, because  $F_3$  is positive,  $u_3$  equals  $u_B$ ,  $u_2$  equals  $u_A$  right; this is the upstream values for these flow rates, alright. That means, what we get is, for cell B, we get  $F_3$  can be written  $u_3$  can be written as u B,  $F_2 u_2$  can be written as u A. Now, remember that, we are not replacing the  $F_3$  with  $F_B$  here or  $F_2$  with  $F_A$ ; you are only replacing, because upwind difference scheme only tells you to replace phi sub e with the upstream values, not the flow rates, right.



only is your  $F_A = F_B$ ; you can also take  $F_2 = F_A = F_B = F_1 = F_3$  right, because this is conservation of mass. Or even if you take  $F_2$  as linear average of  $F_A$  and  $F_B$ ; you will still get both of them equal being you get a  $F_2 = F_A = F_B$ , right.

Now, this is where we can replace the  $F_2, F_3$  that we have here with either  $F_A$  or  $F_B$ , right. So, I can now write this as  $F_B u_B - F_A u_A = A_B(P_2 - P_3)$ , right.

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discrete mom. eqns. for cells A & B

Cell: A:  $F_A u_A = A_A (P_1 - P_2)$

Cell: B:  $F_B u_B - F_A u_A = A_B (P_2 - P_3)$

starred-equations  $F_A u_A^* = A_A (P_1^* - P_2^*)$

$F_B u_B^* = F_A u_A^* + A_B (P_2^* - P_3^*)$

Prime-equations  $F_A u_A' = A_A (P_1' - P_2')$

$F_B u_B' = F_A u_A' + A_B (P_2' - P_3')$

(SIMPLE)

That can be written; that means our momentum equations. So, these are the discrete momentum equations for cells A and B, ok. What we have is  $F_A u_A = A_A(P_1 - P_2)$  and for cell B, we have  $F_B u_B - F_A u_A = A_B(P_2 - P_3)$ , ok. So, how do we construct the star equations here? Starred equations are basically use a guess value for pressure; then the velocity value should be the star values that these equations have to be converge too, alright.

That means, the starred equations for cell A is  $F_A u_A^* = A_A(P_1^* - P_2^*)$  and  $F_B u_B^* = F_A u_A^* + A_B(P_2^* - P_3^*)$ , alright that is given. Then how do we consider the prime equations? Prime equations is basically subtract the star equations from the original equation.

That means you get  $F_A u_A'$  prime, because  $u_A$  minus  $u_A^*$  gives  $u_A'$  equals  $A_A(P_1' - P_2')$  that is the prime equation for cell A. Prime equation for cell B would be  $F_B u_B' = F_A u_A' + A_B(P_2' - P_3')$ , right.

But in this we make the, because of the simple algorithm; the contribution coming from the  $\sum a_{nb}$  prime, that is this term would be taken to be 0, ok. So, essentially this

approximation is coming from simple algorithm, right. This is basically coming from simple algorithm that your  $F_A u'_A$  equal 0, ok.

So, basically this is equal 0 and we also know that  $P_1$  and  $P_3$  are given  $P_1$  is given as 200,  $P_3$  is given as 38 I suppose, right; sorry  $P_1$  is given as 28 and  $P_3$  is given as 0, that means  $P_1$  the pressures are given. So, the pressure corrections are 0. So,  $P_1$  prime equal 0 and  $P_3$  prime equal 0, right. That means, this is 0 and this is 0 and this is taken to be 0, because of the simple approximation, alright.

(Refer Slide Time: 38:09)

$$u'_B = \left(\frac{A_B}{F_B}\right) (P'_2) = d_B P'_2; \quad d_B = \left(\frac{A_B}{F_B}\right)$$

$$\boxed{\begin{aligned} u'_A &= -d_A P'_2 \\ u'_B &= +d_B P'_2 \end{aligned}}$$

velocity corrections in terms of pressure corrections

From the continuity equation:  $F_B - F_A = 0$

$p=1;$   $F'_B - F'_A = F_A^* - F_B^*$

$u'_B A_B - u'_A A_A = F_A^* - F_B^*$

known; mass imbalance for cell 2

So, this is 0 as such; that means we have these things, then we can write this as  $u'_A$  as  $A_A/F_A$ , right. This is what we are calling it as some  $d$  right; remember we had  $\Delta y$  upon the central coefficient a east that we are written as  $d$ ,  $d_e$ . Similarly, we have a prime equals capital  $A_A/F_A$  times  $-P'_2$ .

So, we can write this as  $-d_A P'_2$ , where  $d_A$  is your  $A_A/F_A$  this. Similarly,  $u'_B$  equals  $A_B/F_B$  that is  $A_B/F_B$  times  $P'_2$ . So, this can be written as  $d_B P'_2$ , where  $d_B$  equals  $A_B/F_B$ , ok. That means, we go now velocity corrections for cells A and B in terms of the pressure corrections that is  $P'_2$ .

So, this is your velocity corrections in terms of pressure corrections. Now, these are important, because this is what we need to substitute in the continuity equation. So, but from the continuity equation what we have is, we have  $F_B - F_A = 0$ . So, which of course,

can be decomposed into star and prime values and if the star values are sent to the right hand side; what we get is, we get  $F'_B - F'_A = F_A^* - F_B^*$  right, this is basically sent to the right hand side.

Then a densities given as 1. So, we can write  $F_B$  as  $\rho u_B$  right  $\rho u_A$ ; that means rho is 1. So, we can write this as  $u'_B A_B - u'_A A_A = F_A^* - F_B^*$ , right. So, the right hand side, this term is already known; this is the mass imbalance for cell 2, right. The amount by which the velocities do not satisfy the conservation of mass for cell 2 is the  $F_A^* - F_B^*$  star.

Now, this is not equal to 0; if this is equal to 0, then we have reached convergence, right for momentum equations also right, that is why this is not equal to 0 at the moment. This we have could have computed ok, before coming to this step. Now, we substitute for A B prime u A,  $u'_A$  and  $u'_B$  from these equations. So, substitute for  $u'_B$  as  $d_B P'_2$ , and  $u'_A$  as  $-d_A P'_2$ .

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$$(d_B A_B + d_A A_A) P'_2 = (u_A^* A_A - u_B^* A_B)$$

pressure-correction equation for cell-2  
 Only one cell  
 Using the starred values for velocities we can calculate  $p'_2$

$$p'_2 = \frac{(u_A^* A_A - u_B^* A_B)}{(d_A A_A + d_B A_B)}$$

$$u_A = u_A^* + u'_A = u_A^* - d_A P'_2$$

$$u_B = u_B^* + u'_B = u_B^* + d_B P'_2$$

$$p_2 = p_2^* + (\alpha_p) p'_2$$

*under relax*  
*due to non-linear convection term; momentum equations*

And then write an equation for  $P'_2$ . So, if I substitute that, then what we get is  $u'_B$  equals  $d_B P'_2$ . So, this is basically  $d_B A_B$  and we have this is basically  $-d_A P'_2$ , that becomes a plus  $d_A A_A$  times  $P'_2$ , right that is  $P'_2$  equals on the right hand side we have  $F_A^*$  is rho equals 1. So, this is  $u_A^* A_A$  minus  $u_B^* A_B$  right; because we only know the star values and the cross sectional areas.

That means, we can we know everything on the right hand side; we know the coefficients here, the cross sectional areas are known and the d values are known, that means we can write an equation for pressure correction for cell 2.

So, this is basically the pressure correction equation for cell 2, again we have only, we have only one cell. So, we do not need to solve for Gauss Seidel, rather using the starred values for velocities right; we can calculate  $P'_2$  that can be calculated, fine. So, this is the pressure correction equation.

Now, once you know, once you obtain the pressure correction; you can now correct the velocities using  $u_A = u_A^* + u'_A$ ,  $u'_A$  equals  $-d_A P'_2$ . So, this is  $u_A^* - d_A P'_2$ . Similarly,  $u_B = u_B^* + u'_B$ ; that means,  $u_B^* + u'_B$  is your  $d_B P'_2$  and  $P_2$  equals  $P_2^*$  plus again I use some under relaxation because of the non-linearity of the convection term this time, right.

So, this is basically  $P_2 = P_2^* + \alpha_P P'_2$ . So, owing to the non-linear convection term, we need to also under relax the momentum equations and under relax the pressure while we are correcting it.

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Owing to non-linear convection term; momentum equations

Cell A:  $F_A u_A^* = A_A (P_1^* - P_2^*)$

under-relaxed mom. eqn. for cell A:  $\left(\frac{F_A}{\alpha_u}\right) u_A^* = A_A (P_1^* - P_2^*) + \left(\frac{1-\alpha_u}{\alpha_u}\right) F_A u_A^{**}$

Cell B:  $F_B u_B^* = F_A u_A^* + A_B (P_2^* - P_3^*)$

$\left(\frac{1}{\alpha_u}\right) F_B u_B^* = F_A u_A^* + A_B (P_2^* - P_3^*) + \left(\frac{1-\alpha_u}{\alpha_u}\right) F_B u_B^{**}$

So, now how do we under relax the momentum equations? The original momentum equation, the star equation is  $F_A u_A^* = A_A (P_1^* - P_2^*)$ . So, if have to under relax them, you divide this by alpha and the extra term on the right hand side; thus this becomes  $F_A/\alpha_u$

times  $u_A^*$  equals  $A_A(P_1^* - P_2^*)$  you get  $(1 - \alpha_u)/\alpha_u$  times this quantity that is  $F_A u_A^*$  star ok, basically indicating these terms are already known.

So, that is your under relaxed, under relaxed momentum equation for cell A ok, which you will use when you solve for the guess velocities and guess pressures to calculate the converged velocities at the cells, ok. This is what you will use. Again the momentum equation for cell B was given as  $F_B u_B^*$  star equals  $F_A u_A^*$  plus  $A_B(P_2^* - P_3^*)$  right; remember this is what the original equations we had written, right.

So, we had these two equations right and we wrote the star equations here. Now, we are trying to under relax them and if you were to under relax the cell B; then what you get is basically this is  $F_B u_B^*$ . So, you will get  $1/\alpha_u$  times  $F_B u_B^*$  star equals  $F_A u_A^*$  star plus  $A_B(P_2^* - P_3^*)$  plus you get  $(1 - \alpha_u)/\alpha_u$  times , ok.

So, this is basically your under relaxed equation for cell B, fine. So, again because of the non-linearity of the convection term, we have to do multiple iterations here, so that we converge to a final solution that is driven through continuity satisfying velocity fields by the simple algorithm, alright.

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6.7)  $Q = C \Delta p$  mom. eqn.

$\Delta p =$  pressure drop over the length of the pipe

$C =$  Hydraulic Conductance

$p_1 = 235; p_2 = 230$

$p_4 = 0; p_5 = 40; Q_F = 40$

$C_A = 0.4; C_B = C_D = C_F = 0.2$

$C_C = C_E = 0.1$

The diagram shows a pipe network with nodes 1 through 7. Node 1 is the inlet on the left. Node 2 is at the top, node 3 is at the junction below it, and node 4 is at the bottom. Node 6 is to the right of node 3, and node 5 is at the bottom below it. Node 7 is the outlet on the far right. Flow rates are indicated by arrows: A (right from 1), B (up to 2), C (down to 4), D (right to 6), E (up to 5), and F (right to 7).

Let us look at the final problem from the book that is basically problem 6.7, which is a pipe network; that is let say it distributes water to a residential area, ok. Essentially we have different locations here and the flow through the pipe, the flow rate  $Q$  is given as



some hydraulic conductance  $C$  times the  $\Delta P$ , where  $\Delta P$  is the pressure drop over the length of the pipe, ok.

This is basically the  $P$  upstream minus  $P$  downstream, that is the pressure drop over the length the  $L$  and  $C$  is the hydraulic conductance and  $Q$  is the flow rate ok. And the pipe network is shown here; so the locations dark circles here 1, 2, 3 all the way to 7 are the locations where the pressure is stored. And the arrows here denote the direction of the flow and there also the locations where the velocities are stored. So, for example, the velocities stored as at A, B all the way to F.

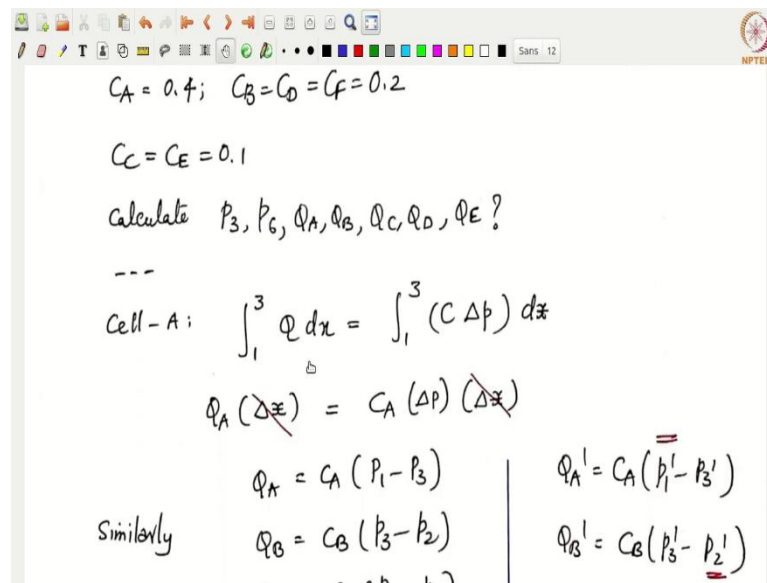
Now, few pressure values are given that is  $P_1, P_2, P_4, P_5$  is given. So, all these things are given; 3, 6 and 7 are not given, and the flow rate also through F is given. So,  $Q_F$  is given this is 40 and the hydraulic conduction is given for all of them; that is  $C_A$  is given as 0.4,  $C_B$  D F that is B D F all these three are 0.2,  $C_C$  and  $C_E$  are given as 0.1 all the hydraulic conductance given.

So, we were asked to calculate what is the pressure  $p_3, p_6$  and what is the value for  $Q_A, Q_B, Q_C, Q_D$  and  $Q_E$ . We need to calculate what is A, B, C, D and E these flow rates is what you need to calculate. And the given equation is only the  $Q$  equals  $C$  times the delta  $p$ . Now, what equation is this?

This is momentum equation or this is now what kind of an equation this is the? What do we take this as? We should take this as basically momentum equation is not it; because you have kind of an integrated momentum equation ok, where the flow rate equals  $C$  times  $\Delta P$ .

So,  $\frac{dP}{dx}$  is not given similarly the  $\frac{dP}{dx}$  of this guy is not given. So, this is the momentum equation; that means we have to solve for this equation at locations A, B, C all the way to F right that is what we have to do, alright. So, we have to calculate these two pressures and the flow rates for A to E alright; that means we know that this is momentum equation.

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$C_A = 0.4; C_B = C_D = C_F = 0.2$   
 $C_C = C_E = 0.1$   
 Calculate  $P_3, P_6, Q_A, Q_B, Q_C, Q_D, Q_E?$   
 ---  
 Cell-A:  $\int_1^3 Q dx = \int_1^3 (C \Delta p) dx$   
 $Q_A (\Delta x) = C_A (\Delta p) (\Delta x)$   
 $Q_A = C_A (P_1 - P_3)$  |  $Q_A' = C_A (P_1' - P_3')$   
 Similarly  $Q_B = C_B (P_3 - P_2)$  |  $Q_B' = C_B (P_3' - P_2')$

So, if you were to write for cell A, cell A the limits are 1 and 3. So, you have to integrate 1 to 3,  $Q dx$  equals 1 to 3,  $C \Delta P dx$ , right. Now, what is  $Q$ ?  $Q$  is the flow rate what in; under what term do you want to call this as, what type of term is this? This is basically like a source term right; because  $Q$  is kind of constant for the entire cell and the cell centroid value is what you want to take it as a representative, right.

So,  $Q$  would be  $Q_A$  and will be constant, so integral  $dx$  will be  $\Delta x$ . So, this will be  $\Delta x$  equals  $C$  you can evaluate the cell centroid that is  $C_A$ . What about  $\Delta P$ ?  $\Delta P$  is also you know constant. So,  $C_A \Delta P$  times integral  $dx$  would be  $\Delta x$  right, basically  $x_3$  minus  $x_1$ ,  $x_3$  minus  $x_1$ . So, these two  $\Delta x$  get cancel. So, what you get is  $Q_A$  equals  $C_A$  times  $\Delta p$ . And what is  $\Delta P$ ?  $\Delta P$  is the pressure drop across the length and the length is for 1, 2, 3, right.

So, along this much length right; that means  $P_1$  minus  $P_3$  would be  $\Delta P$  for length a right for the vector A. So, that means, this is basically  $Q_A$  equals  $C_A$  times  $P_1$  minus  $P_3$ ; similarly we can write the equations. So, what will be  $Q_B$ ?  $Q_B$  would be equal to  $C_B$  times  $P_3$  minus  $P_2$  right, because the flow is going in that way.

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discrete mom. eqns. for cells A through F

Similarly

$$Q_A^* = C_A (P_1^* - P_3^*)$$

$$Q_B = C_B (P_3 - P_2)$$

$$Q_C = C_C (P_4 - P_3)$$

$$Q_D = C_D (P_5 - P_6)$$

$$Q_E = C_E (P_5 - P_6)$$

$$Q_F = C_F (P_6 - P_7)$$

starred equations

$$Q_A' = C_A (P_1' - P_3')$$

$$Q_B' = C_B (P_3' - P_2')$$

$$Q_C' = C_C (P_4' - P_3')$$

$$Q_D' = C_D (P_3' - P_2')$$

$$Q_E' = C_E (P_5' - P_6')$$

$$Q_F' = C_F (P_6' - P_7')$$

prime equations.

Similarly, what would be  $Q_C$ ?  $Q_C$  equal to  $C_C$  times  $P_4$  minus  $P_3$ . So, that is  $Q_C$  equals  $C_C$  times  $P_4$  minus  $P_3$ . And what would be  $Q_D$ ?  $Q_D$  would be  $C_D$  times  $P_3$  minus  $P_6$ . So, that is your  $Q_D$  right;  $Q_D$  equal  $C_D$  times  $P_3$  minus  $P_6$ . And  $Q_E$  would be  $C_E$  times  $P_5$  minus  $P_6$ . So, that is  $Q_E$  is  $C_E$  times  $P_5$  minus  $P_6$ . And similarly you can write what is  $Q_F$  equals  $C_F$  time  $P_6$  minus  $P_7$ .

So, these are the now the discrete momentum equations for cells A through F, right ok. Now, once you know these basically these are the starred equations right, these are the starred equation; if I have to put star here for  $P_1^*$  and  $P_3^*$  and then what I obtain here is your  $Q_A^*$  right, this is your  $Q_A^*$ .

Now, if you subtract of the starred equations from the non-starred equations; what is get is the prime equation. So, we can write the prime equations on the right hand side; those are nothing, but  $Q_A'$  equals  $C_A$  times  $P_1'$  minus  $P_3'$ . So, it is kind of easy to see from these equations how to write them and  $Q_B'$  equals  $C_B$  times  $P_3'$  minus  $P_2'$ .

Similarly,  $Q_C'$  equals  $C_C$  times  $P_4'$  minus  $P_3'$ , and  $Q_D'$  equals  $C_D$  times  $P_3'$  minus  $P_6'$ , and  $Q_E'$  equals  $C_E$  times  $P_5'$  minus  $P_6'$ , and  $Q_F'$  equals  $C_F$  times  $P_6'$  minus  $P_7'$ , ok. So, we got all the pressure correction essentially prime equations in terms of; we do not have velocities now, but we have flow rates right, essentially  $Q$  is like our velocity. So, we kind of related the velocity corrections or flow rate corrections in terms of pressure corrections, alright.

So, now what is the step that follows? Basically you have to look with the continuity equation; but we were not given continuity equation right, because the only equation we are given is  $Q$  equals  $C$  times  $\Delta P$ . But what are the locations where do we have to apply continuity equations?

We have to apply continuity equation at the pressure cells or the primary cell. That means, we have to apply this at 1, 2, 4, 3, 6, 5, 7, right; but again we do not have to apply at 1, 2, 4, 5, because 1, 2, 4, 5 the values are already given. So, we need to apply only at 3 and 6 right and at 7.

So, but at 7 we do not have to apply; because the flow rate is already given, so that is flowing in. So, we need to apply continuity equation at 3 and 6. What would be the continuity equation at 3? I mean continuity equation is basically at 3 is whatever that is flowing in minus whatever that is flowing out should be equal to 0.

That means, for cell 3, the conservation of mass is  $Q_A$  plus  $Q_C$  minus  $Q_B$  minus  $Q_D$  equal to 0 that is conservation of mass for cell 3; that is  $Q_A$  plus  $Q_C$  minus  $Q_B$  minus  $Q_D$  equal to 0. And the continuity equation for 6 would be  $Q_D$  plus  $Q_E$  minus  $Q_F$  equal to 0, right. So, those are the continuity equations.

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Continuity equation: Cell-3:  $Q_A + Q_C - Q_B - Q_D = 0$

$$Q_A' + Q_C' - Q_B' - Q_D' = Q_B^* + Q_D^* - Q_A^* - Q_C^*$$

known

$$C_A(p_1' - p_3') + C_C(p_4' - p_3') - C_B(p_3' - p_2') - C_D(p_3' - p_6') = Q_B^* + Q_D^* - Q_A^* - Q_C^*$$

$$p_3'(-C_A - C_B - C_C - C_D) + p_6'(C_D) = Q_B^* + Q_D^* - Q_A^* - Q_C^*$$

Now, that means, we can write the continuity equations for pressure cells, that is for cell 3 is  $Q_A$  plus  $Q_C$  minus  $Q_B$  minus  $Q_D$  equal to 0. Now, this can be decomposed into star and prime quantities and the star values can be sent to the right hand side.

So, what you get is  $Q_B^*$  plus  $Q_D^*$  minus  $Q_A^*$  minus  $Q_C^*$  on the right hand side, which is basically known right from the converged star values. And on the left hand side, we are left with  $Q'_A$  plus  $Q'_C$  minus  $Q'_B$  minus  $Q'_D$ , right alright. So, we are left with this.

Now, we can substitute for  $Q'_A$   $Q'_C$   $Q'_B$  and  $Q'_D$  from the equations we have derived here, right. So, we will substitute for them; that means we substitute  $Q'_A$  equals  $C_A$  times  $P'_1$  minus  $P'_3$ ,  $Q'_C$  as  $C_C$  times  $P'_4$  minus  $P'_3$  minus  $Q'_B$  as  $C_B$  times  $P'_3$  minus  $P'_2$ , and  $Q'_D$  as  $C_D$  times  $P'_3$  minus  $P'_6$  equals everything on the right hand side.

Now, we also realize that, because the pressure values are given at locations 1, 2, 4 and 5; the p primes at these locations are 0 right, we do not need to do any pressure correction there. So, the pressure correction is 0. So, as a result  $P'_1$  is 0;  $P'_4$  is also 0,  $P'_2$  is also 0 and these two are not 0, ok.

That means, we can write collect  $P'_3$  terms. So,  $P'_3$  equals minus  $C_A$  minus  $C_B$  minus  $C_C$  and minus  $C_D$  that is what we get. And we have plus p 6 prime that is coming from here, which is  $P'_6 C_D$  equals something on the right hand side that is basically  $Q_B^*$  plus  $Q_D^*$  minus  $Q_A^*$  minus  $Q_C^*$ , ok

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pressure correction equation for cell 3  
that also contains contribution from cell 6  $\Rightarrow \rightarrow \textcircled{1}$

Cell-6:

$$Q_D + Q_E - Q_F = 0$$

$$Q_D^1 + Q_E^1 - Q_F^1 = Q_F^* - Q_D^* - Q_E^* \text{ known}$$

$$C_D(p'_3 - p'_6) + C_E(p'_3 - p'_6) - 0 = Q_F - Q_D^* - Q_E^*$$

$$p'_3(C_D) + p'_6(-C_D - C_E) = Q_F - Q_D^* - Q_E^* \rightarrow \textcircled{2}$$

Solve for  $p'_3$  and  $p'_6$  ...

So, this is now your pressure correction equation right; this is very different from what we had till now, till now we had only one pressure cell, now we have two pressure cells that is C 3 and 6. So, this is pressure correction equation for cell 3 that also contains contribution from cell 6 right, that is  $P'_6$  is also there, ok.

So, we have two unknowns here, but this is one of the equations; the other equation will come from cell 6. So, for cell 6 what we have is, we have  $Q_D$  plus  $Q_E$  minus  $Q_F$  equal to 0 that is the continuity equation for cell 6,  $Q_D$  plus  $Q_E$  minus  $Q_F$  equal to 0, right. So, if you were to again write that equation, then we have decompose this into star and primes.

The equation we get is  $Q'_D$  plus  $Q'_E$  minus  $Q'_F$  equal to  $Q'_F$  star minus  $Q_D^*$  sorry  $Q_F^*$  minus  $Q_D^*$  minus  $Q_E^*$ . So, the right hand side thing here is already known. And because  $Q'_F$  is basically given;  $Q_F$  is given as 40,  $Q'_F$  would be equal to 0 right, because this is given this is equal to 0.

And we can substitute for  $Q'_D$  in terms of pressure corrections that is  $C_D$  times  $P'_3$  minus  $P'_6$  plus  $C_E$  times  $P'_5$  minus  $P'_6$  minus this is 0 equals;  $Q_F^*$  is nothing, but  $Q_F$ , right. So, this is  $Q_F$  minus  $Q_D^*$  minus  $Q_E^*$  which is already known and  $P_5$  is given. So, as a result if  $p_5$ s prime is this is 0, ok.

So, this is 0; that means we again have equation in terms of  $P'_3$  and  $P'_6$ . So,  $P'_3$  times  $C_D$  plus  $P'_6$  times minus  $C_D$  minus  $C_E$  equals  $Q_F$  minus  $Q_D^*$  minus  $Q_E^*$ . So, this is our other pressure correction equation for  $P'_3$  and  $P'_6$ . So, we have this is a second equation and the unknowns are  $P'_3$  and  $P'_6$ .

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Solve for  $p_3'$  and  $p_6'$  ...

$$p_3 = p_3^* + p_3'$$

$$p_6 = p_6^* + p_6'$$

Iterate?  
Linear  
No need to iterate  
converge in 1 iteration!

Programs; try to run the programs for these three problems.

2 eqns and 2 unknowns.

$$Q_A = Q_A^* + Q_A' = Q_A^* - C_A p_3'$$

$$Q_B = Q_B^* + Q_B' = Q_B^* + C_B p_3'$$

$$Q_C = Q_C^* + Q_C' = Q_C^* - C_C p_3'$$

$$Q_D = Q_D^* + Q_D' = Q_D^* + C_D (p_3' - p_6')$$

$$Q_E = Q_E^* + Q_E' = Q_E^* - C_E p_6'$$

So, we have two equations and two unknowns. Of course, in a traditional sense, we would have solved for Gauss Seidel here right for solving the pressure correction equation; but here we have 2 equations and 2 unknowns, right. So, we do not, we do not have to solve for Gauss Seidel; we can directly solve for 2 equations 2 unknowns.

So, solve for  $P_3'$  and  $P_6'$ , ok. Then once you know the pressure corrections, you can update the pressures using  $P_3 = P_3^* + P_3'$ . And  $P_6 = P_6^* + P_6'$  and then we correct the flow rates right; essentially  $Q_A$  equals  $Q_A^*$  plus  $Q_A'$ , where  $Q_A'$  equals minus  $C_A$  times  $P_3'$ , because the other contribution of  $P_1'$  is 0.

Similarly,  $Q_B$  equals  $Q_B^*$  plus  $C_B$  times  $P_3'$ ,  $Q_C$  equals  $Q_C^*$  minus  $C_C$  times  $P_3'$ , and  $Q_D$  equals  $Q_D^*$  plus  $C_D$  times  $P_3'$  minus  $P_6'$ . And finally,  $Q_E$  equals  $Q_E^*$  plus  $Q_E'$ , for which we can write minus  $C_E$  times  $P_6'$ ; these are basically the same equations we have derived before.

Only thing is that we have now set these underlined quantities to 0; because those are, those corrections are all 0, because their boundary conditions for pressure are given. Now, what you see; you got one, you got a you corrected your flow rates using the flow rate corrections.

Now, what about how many times? So, do we need to iterate here? Do we need to iterate? Because at this point our solution satisfies the flow rates are satisfied; but what about the momentum equation, is momentum equation linear or not linear? Momentum equation is

linear; that means we do not have to iterate, because whatever in one iteration; it will basically converge, right.

Because, the momentum equation is linear right, the pressure corrections only will affect the flow rate. So, because this is linear, we do not need to iterate right even; it will just converge in one iteration, ok, so, that we will see when we try to solve these problems using a code, ok. So, basically that is all for today. So, in the next lecture, so we will look at, basically we will look at the corresponding programs. And we will try to run the programs for these three problems.

So, it is, it will be good if you can keep these notes handy, ok, so that we can refer to these equations and then look at the program, try to run the program and see and obtain the results for each of these problems, alright. So, I am going to stop here; if you have any questions, send them to me through email ok, alright.

Thank you, talk to you in the next lecture.