

Concepts of Thermodynamics
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Lecture – 04
Introduction to Property Tables

Today, we will see that how to deal with the properties of pure substances for identifying various thermodynamic states. What we have discussed earlier to summarize that we can say that properties are signatures of states right. So, if you have a thermodynamic state, the thermodynamic state is designated by a combination of thermodynamic properties. If it is a simple compressible pure substance, it requires two independent intensive thermodynamic properties to specify the state of the system.

So, condition of a system designated by its properties is called as the state of the system. So, when we say that it means that if we can identify two independent intensive thermodynamic properties, we will be in a position to identify the state; that means, all other properties whatever are relevant can be obtained from that. How do you obtain those properties? So, this is a very important concept to realize that in school level most of you have done some kind of thermodynamics where the properties were dictated by the ideal gas type of relationships.

For example, for an ideal gas you can write $p v$ equal to nRT . So, when you write that, what you are essentially describing is an equation of state where pressure, volume and temperature are related with each other. So that means, if you specify pressure and volume the third property which is temperature is automatically defined by that equation. In many practical scenarios the substance is not an ideal gas. When it is not an ideal gas you cannot use may be in certain cases for non-ideal substances such equations of states are available, some are empirical, some are not.

But, in general such a simple equation of state which is typically like the ideal gas equation of state, will not work for a substance which is more practical than an ideal gas. So, if it is like that then how do you determine the properties that is an important question. And, that is an important situation very challenging situation that most of the students face in working out problems in thermodynamics where the properties are not the properties of ideal gases.

So, what would you do? So, for such a scenario we either have an equation of state which is more complex than the ideal gas equation of state which defines the relationship between properties. That means, if you give two independent intensive properties as input the third property will come as an output from that equation may be a complex equation. But, where pressure is a function of temperature and density in some way or the other or temperature is a function of pressure and density in some way or the other.

So, these things are there. However, it is very convenient if all these data points for a particular substance are summarized or tabulated in the form of thermodynamic property tables. And, today we will try to work out examples where we will illustrate how to use the thermodynamic tables. I would like to emphasize here is that thermodynamics education has gone through a shift of paradigm, traditionally and even when I was myself an undergraduate student we use to follow the property tables very judiciously to identify the state points.

However, over the past few years there has been an emerging trend of using computerized data tables. That means, if you give the properties or give two independent properties as input the third property which is a function of those two properties; we will come out automatically as a part of the software instead of having to look into the table. So, that kind of paradigm has come up recently; it does not change the concepts in thermodynamics, but it changes the approach in which you may possibly solve a problem. So, in this course what we have design is that we will consider both these approaches.

So, one the traditional approach where, looking into the table is important and I will tell you that there is a benefit of the traditional approach. The benefit of the traditional approach is that you can visualize very nicely that what is the physical state of the system; is it two phase system, is it superheated system, is it a sub cooled system. These things you can nicely visualize from the tabular information. The computerized system the advantages that despite the fact that it does not give you an easy visualization until and unless you plot using the computer generated data; you can work out problems relatively quickly and elegantly without making the toil of looking into the property tables in the hard form.

So, there are advantages and disadvantages. I will not get into the debate of which one is a better method and which one is not so convenient. These both these approaches have their own merits and possibly some demerits also. And, I will straight away start helping you out to see that to understand that how the property tables look and how the property tables can be used to solve problems.

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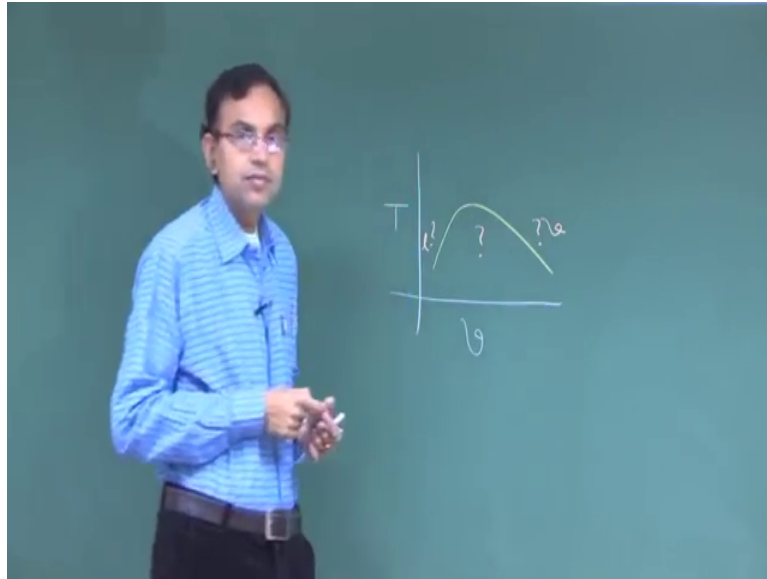


STEAM TABLES

So, if you look into the property tables there are property tables of various substances and many of the substances are actually phase changing substances. That means, given a heat transfer to the system we will see later on what is heat and all, but we can qualitatively understand that by transferring heat you are energizing the molecules of the system. And, then the molecules from the liquid phase for example, can go to the vapor phase or from solid phase can go to the liquid phase. So, this kind of phase changing substances their properties can be nicely tabulated in the form of a structure table.

Why we are interested in such substances because, water one of the most common engineering fluids is of substance of that type. So, properties of water are described or enumerated in the form of tables known as steam tables. So, I would like to explain you first that how the steam tables look and how to look into the properties through steam tables. So, before getting into the steam tables and how do they look? I would like to give you conceptual description of what we are talking about.

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So, let us say that we are interested to plot one state point in a $p-v$ diagram or a $T-v$ diagram whatever. So, when we are interested to so, let us say for example, this is T this is v temperature specific volume diagram. So, for a substance like water you have a diagram like this; dome shaped region below which you have the change of phase as you heat it from liquid to vapor. So, this is let me write it in symbols. So, on this side it is liquid, on this side it is vapor, and in between there is a liquid to vapor transition as you heat the material or heat the fluid. When you have your data point or a state point for which the temperature and pressure is beyond this that is called a supercritical fluid and that does not pass through this phase change process.

So, the first question that given a data given a set of properties where does the state point lie. Does it lie here? Does it lie here or does it lie here? This is the first question that you might be interested to answer before solving a problem. This is state this is like you know step 0 of understanding thermodynamics. We have not yet started looking into thermodynamics, but this is the absolutely essential for solving problems in thermodynamics. So, which where is the state point lie, how do you understand that?

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Example Problem

Water vapor initially at 3 MPa and 300 °C (state 1) is contained within a piston cylinder assembly. The water is cooled at constant volume until its temperature reaches 200 °C (state 2). The water is compressed isothermally to a state when pressure is 2.5 MPa (state 3). Locate state 1, 2 and 3 on a T - v and p - v diagram. Determine specific volume at state 1, 2 and 3 and the quality at state 2.

Steam table data

Saturated water vapor table

Press. (kPa)	Temp. (°C)	Specific Volume, m ³ /kg			Internal Energy, kJ/kg		
		Sat. Liquid v_f	Evap. v_{fg}	Sat. Vapor v_g	Sat. Liquid u_f	Evap. u_{fg}	Sat. Vapor u_g
850	172.96	0.001118	0.22586	0.22698	731.25	1847.45	2578.69
900	175.38	0.001121	0.21385	0.21497	741.81	1838.65	2580.46
950	177.69	0.001124	0.20306	0.20419	751.94	1830.17	2582.11
1000	179.91	0.001127	0.19332	0.19444	761.67	1821.97	2583.64
1100	184.09	0.001133	0.17639	0.17753	780.08	1806.32	2586.40
1200	187.99	0.001139	0.16220	0.16333	797.27	1791.55	2588.82
1300	191.64	0.001144	0.15011	0.15125	813.42	1777.53	2590.95
1400	195.07	0.001149	0.13969	0.14084	828.68	1764.15	2592.83
1500	198.32	0.001154	0.13062	0.13177	843.14	1751.3	2594.5
1750	205.76	0.001166	0.11232	0.11349	876.44	1721.39	2597.83
2000	212.42	0.001177	0.09845	0.09963	906.42	1693.84	2600.26
2250	218.45	0.001187	0.08756	0.08875	933.81	1668.18	2601.98
2500	223.99	0.001197	0.07878	0.07998	959.09	1644.04	2603.13
2750	229.12	0.001207	0.07154	0.07275	982.65	1621.16	2603.81
3000	233.90	0.001216	0.06546	0.06668	1004.76	1599.34	2604.10
3250	238.38	0.001226	0.06029	0.06152	1025.62	1578.43	2604.04

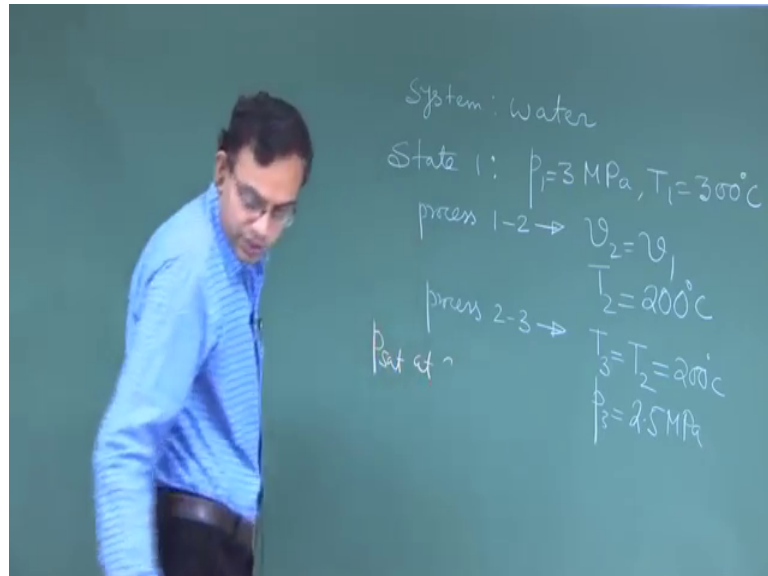
So, to understand that we can refer to specific problem: and then we can try to solve the problem and through that problem we will learn how to use the table. So, for that I will refer to this example problem. So, the problem is described in the slide and we will of course, share these slides with you as a part of supplementary material of this course. But, you can note this problem down so that it helps you to you know do a pen and paper solution of this problem.

So, let me go through the problem statement first. Water vapor initially at 3 MPa 300 degree centigrade which is state 1 is contained within a piston cylinder assembly. The water is cooled at constant volume until its temperature reaches state 2 which is 200 degree centigrade. And, the water is compressed isothermally to a state when the pressure is 2.5 MPa. Locate state 1, 2 and 3 on T v and p v diagram. Determine the specific volumes at state 1, 2 and 3 and quality at state 2. This problem I will do in a very different way. So, I will give you the idea of how to identify the state points.

You have to generate the data from the table and this will be your first homework problem for this particular course. So, let us so whenever there is a problem in thermodynamics. See thermodynamics is many times a very challenging subject to students, because the problem solution is not very structured. Every problem has a different way of looking into it, but we can try to structure this to the extent possible; so,

that it helps you out. So, first is water vapor initially at so, let me look into the properties. So, water vapor initially at 3 MPa 300 degree centigrade so, state 1.

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So, the system thermodynamic system is water state 1 3 MPa and 300 degree centigrade. So, p_1 is 3 mega Pascal T_1 is 300 degree centigrade ok; then the process from 1 to 2, what is the kind of process? It is given, it is cooled in a constant volume process. The process is such that v_2 equal to v_1 see it is a control mass system where the mass is constant.

So, if the total volume is constant and mass is constant; that means, specific volume is also constant. We will discuss later on that why specific volume is considered to be such an important property instead of its inverse which is density in thermodynamics. Why we use specific volume so, commonly instead of using density of course, density is just inverse of the specific volume so, we could use the density also. But specific volume why it is so, convenient to use specific volume as a property and density not so, much convenient while working out problems in thermodynamics; we will discuss about that.

So, the process 1 to 2 v_2 is equal to v_1 and then this is the other information remember that we require two independent properties because; water is a simple compressible pure substance. So, we require two independent properties for specifying its state. So, what is T_2 ? T_2 is given as 200 degree centigrade. It is cooled from 300 to 200 degree centigrade. Then from state 2 to state 3, what it does? The water is compressed

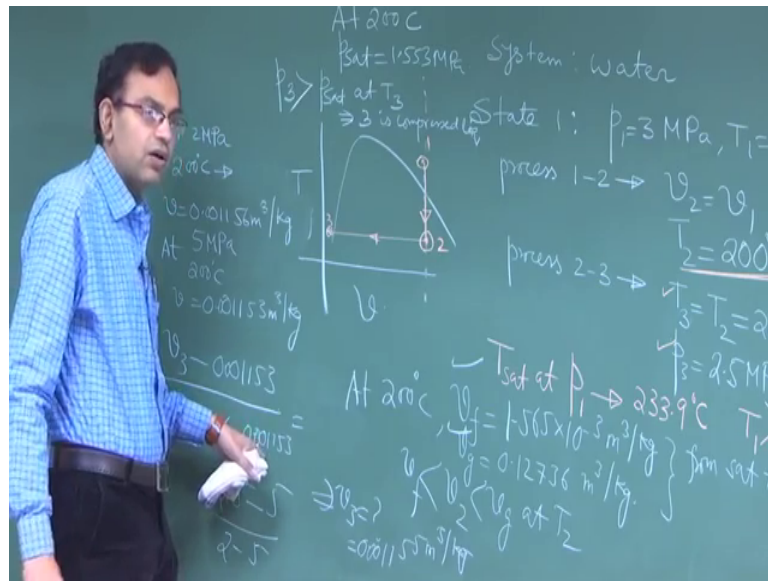
isothermally to a state 3. So, process 2 to 3 T_3 is equal to T_2 and which is 200 degree centigrade and p_3 is equal to 2.5 mega Pascal.

What you have to do for this problem is simply identify the state points on a $p-v$ and $T-v$ diagram and maybe the processes and determine the specific volume at 1, 2 and 3 and quality at state 2 ok. So, let us try to look into this problem. I will do the initial problems very slowly; so, that you can understand that how to solve these problems by looking into the property tables; state 1 3 or 3 MPa T_3 300 degree centigrade. Now, can you tell whether this is liquid water, liquid plus vapor or superheated vapor; how can you tell this. So, let us look into the steam table.

So, just look into the table which is given in the slide. So, the first portion of the table is saturated water vapor table ok. So, in the saturated water vapor table let us look into the data of 3 mega Pascal, 3 mega Pascal is 3000 kilo Pascal. So, if you look here you will see that the first column is like pressure, second column is temperature. See in the two phase region if you defined the value of pressure the temperature is also defined automatically.

Because the saturation pressure and saturation temperature they are unique functions of each other. So, when you have saturation pressure as 300 3000 kilo Pascal, its corresponding saturation temperature is 233.9 degree centigrade, you look it from the table. So, when you have this as 233.9 degree centigrade what is your given temperature. So, let us write this p_{sat} at sorry T_{sat} at p_1 , what is that. It is 233.9 degree centigrade ok.

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Your T_1 is greater than this; that means, it has crossed the saturation temperature limit. This implies that it is in the superheated vapor region. So, when it is in the superheated vapor region, this table which is the saturated water vapor table you can see here this saturated water vapor table will not work anymore. You have to consider the superheated table, but even if it is a superheated data point your first check is from the saturated water table to figure out whether it is actually superheated or not. So, once you get that data what do you do is, you find out you look into the superheated vapor table.

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Steam table data								
Temp. (°C)	v (m ³ /kg)	u (kJ/kg)	h (kJ/kg)	s (kJ/kg-K)	v (m ³ /kg)	u (kJ/kg)	h (kJ/kg)	s (kJ/kg-K)
3000 kPa (233.90°C)				Superheated water vapor				
4000 kPa (250.40°C)								
Sat.	0.06668	2604.10	2804.14	6.1869	0.04978	2602.27	2801.38	6.0700
250	0.07058	2644.00	2855.75	6.2871	—	—	—	—
300	0.08114	2750.05	2993.48	6.5380	0.05884	2725.33	2960.68	6.3614
350	0.09053	2843.66	3115.25	6.7427	0.06645	2826.65	3092.43	6.5820
Saturated water vapor								
Temp. (°C)	Press. (kPa)	Specific Volume, m ³ /kg			Internal Energy, kJ/kg			
		Sat. Liquid v_f	Evap. v_{fg}	Sat. Vapor v_g	Sat. Liquid u_f	Evap. u_{fg}	Sat. Vapor u_g	
195	1397.8	0.001149	0.13990	0.14105	828.36	1764.43	2592.79	
200	1553.8	0.001156	0.12620	0.12736	850.64	1744.66	2595.29	
205	1723.0	0.001164	0.11405	0.11521	873.02	1724.49	2597.52	
Temp. (°C)	v (m ³ /kg)	u (kJ/kg)	h (kJ/kg)	s (kJ/kg-K)	Compressed liquid water			
					v (m ³ /kg)	u (kJ/kg)	h (kJ/kg)	s (kJ/kg-K)
2000 kPa (212.42°C)					5000 kPa (263.99°C)			
160	0.001101	674.14	676.34	1.9410	0.001099	672.61	678.10	1.9374
180	0.001127	761.46	763.71	2.1382	0.001124	759.62	765.24	2.1341
200	0.001156	850.30	852.61	2.3301	0.001153	848.08	853.85	2.3254

So, in the superheated vapor table if you have the pressure as 3 MPa which is here or 3000 kilo Pascal at 300 degree centigrade, you get what is the specific volume. Some other properties are there internal energy, enthalpy entropy. Whenever we will require these properties we will discuss, but for this problem it is the specific volume that is required. So state 1, so, we can simply write that from superheated table from superheated water table you have the specific volume at state 1 is 0.08114 0.0811 say let us stop here meter cube per kg.

So, I will draw one of the diagram say T v diagram. So, state 1 is someone here this is what you can visualize. From state 1 to state 2 you have v 2 is equal to v 1 which is this one and T 2 is 200 degree centigrade. So, the question is, is it still in the superheated or it has come to saturated. What is the on which line the point state point 2 will lie, if you draw a vertical line. Somewhere on this it will lie if because, it is cooled it will be down. But, the question is down where beyond this line or below this line. So, for that again you have to look into the table at 200 degree centigrade. So, let us try to look into that, the saturated table so, 200 degree centigrade so.

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Steam Table – Saturated Water^[1]

Temp. (°C)	Press. (kPa)	Specific Volume, m ³ /kg			Internal Energy, kJ/kg		
		Sat. Liquid v_f	Evap. v_{fg}	Sat. Vapor v_g	Sat. Liquid u_f	Evap. u_{fg}	Sat. Vapor u_g
0.01	0.6113	0.001000	206.131	206.132	0	2375.33	2375.33
5	0.8721	0.001000	147.117	147.118	20.97	2361.27	2382.24
10	1.2276	0.001000	106.376	106.377	41.99	2347.16	2389.15
15	1.705	0.001001	77.924	77.925	62.98	2333.06	2396.04
20	2.339	0.001002	57.787	57.787	83.94	2318.98	2402.91
25	3.169	0.001003	43.383	43.393	104.86	2304.90	2409.76
30	4.246	0.001004	32.8922	32.8932	125.77	2290.81	2416.58
35	5.628	0.001006	25.2148	25.2158	146.65	2276.71	2423.36
40	7.384	0.001008	19.5219	19.5229	167.53	2262.57	2430.11
45	9.593	0.001010	15.2571	15.2581	188.41	2248.40	2436.81
50	12.350	0.001012	12.0308	12.0318	209.30	2234.17	2443.47
55	15.758	0.001015	9.56734	9.56835	230.19	2219.89	2450.08
60	19.941	0.001017	7.66969	7.67071	251.09	2205.54	2456.63
65	25.03	0.001020	6.19554	6.19656	272.00	2191.12	2463.12
70	31.19	0.001023	5.04114	5.04217	292.93	2176.62	2469.55
75	38.58	0.001026	4.13021	4.13123	313.87	2162.03	2475.91
80	47.39	0.001029	3.40612	3.40715	334.84	2147.36	2482.19
85	57.83	0.001032	2.82654	2.82757	355.82	2132.58	2488.40
90	70.14	0.001036	2.35953	2.36056	376.82	2117.70	2494.52
95	84.55	0.001040	1.98082	1.98186	397.86	2102.70	2500.56
100	101.3	0.001044	1.67185	1.67290	418.91	2087.58	2506.50

[1] BORIGNAKKE, C., SONNTAG, R. E., SOM, Fundamental of Thermodynamics, Seventh Edition, Wiley Publication

So, 200 degree centigrade I do not have the data point with me here in this table. It is up to 100 degree centigrade it is given because this is just way of giving you an idea how to do that. So, at 100 degree centigrade for example, you have v f and v g. If it is in the two

phase region at 100 degree centigrade this is v f where, I have pointed the pointer and this is what is v g. So, if your v is between v f and v g then it is in the two phase region.

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Steam Table – Saturated Water (Pressure Table)_[2]

Press. (kPa)	Temp. (°C)	Specific Volume, m ³ /kg			Internal Energy, kJ/kg		
		Sat. Liquid v_f	Evap. u_{fg}	Sat. Vapor v_g	Sat. Liquid u_f	Evap. u_{fg}	Sat. Vapor u_g
0.6113	0.01	0.001000	206.131	206.132	0	2375.3	2375.3
1	6.98	0.001000	129.20702	129.20802	29.29	2355.69	2384.98
1.5	13.03	0.001001	87.97913	87.98013	54.70	2338.63	2393.32
2	17.50	0.001001	67.00285	67.00385	73.47	2326.02	2399.48
2.5	21.08	0.001002	54.25285	54.25385	88.47	2315.93	2404.40
3	24.08	0.001003	45.66402	45.66502	101.03	2307.48	2408.51
4	28.96	0.001004	34.79915	34.80015	121.44	2293.73	2415.17
5	32.88	0.001005	28.19150	28.19251	137.79	2282.70	2420.49
7.5	40.29	0.001008	19.23674	19.23775	168.76	2261.74	2430.50
10	45.81	0.001010	14.67254	14.67355	191.79	2246.10	2437.89
15	53.97	0.001014	10.02117	10.02218	225.90	2222.83	2448.73
20	60.06	0.001017	7.64835	7.64937	251.35	2205.36	2456.71
25	64.97	0.001020	6.20322	6.20424	271.88	2191.21	2463.08
30	69.10	0.001022	5.22816	5.22918	289.18	2179.22	2468.40
40	75.87	0.001026	3.99243	3.99345	317.51	2159.49	2477.00
50	81.33	0.001030	3.23931	3.24034	340.42	2143.43	2483.85
75	91.77	0.001037	2.21607	2.21711	394.29	2112.39	2496.67
100	99.62	0.001043	1.69296	1.69400	417.33	2088.72	2506.06

[2] BORGNAKKE, C., SONNTAG, R. E., SOM, *Fundamental of Thermodynamics, Seventh Edition, Wiley Publication*

Similarly, at 200 degree centigrade you will have some v f and some v g.

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Steam Table – Superheated Water Vapor_[3]

Temp (°C)	$P = 10 \text{ kPa (45.81 °C)}$				$P = 50 \text{ kPa (81.33 °C)}$			
	v (m ³ /kg)	u (kJ/kg)	h (kJ/kg)	s (kJ/kg K)	v (m ³ /kg)	u (kJ/kg)	h (kJ/kg)	s (kJ/kg K)
Sat.	14.6725	2437.89	2584.63	8.1501	3.2403	2483.85	2643.87	7.8839
30	14.8020	2443.87	2592.36	8.1749	—	—	—	—
100	17.1961	2515.50	2687.46	8.4479	3.41833	2511.41	2682.52	7.6947
150	19.31251	2587.86	2782.99	8.6981	3.89327	2585.41	2766.08	7.9490
200	21.82867	2661.27	2879.52	8.9037	4.36596	2659.85	2851.44	8.1239
250	24.13530	2735.95	2977.31	9.1062	4.83045	2734.97	2935.99	8.3055
300	26.44608	2812.06	3076.51	9.2812	5.28931	2811.33	3015.52	8.4572
400	31.68252	2968.89	3279.51	9.6076	6.20929	2968.43	3279.89	8.8641
500	35.67996	3102.26	3489.05	9.8977	7.13364	3131.94	3488.62	9.1545
600	40.29488	3202.45	3705.40	10.1608	8.05748	3302.22	3705.19	9.4377
700	44.81652	3479.63	3928.73	10.4028	8.98104	3479.15	3928.51	9.6999
800	49.52590	3663.84	4159.10	10.6281	9.90444	3663.70	4158.92	9.9432
900	54.14137	3855.03	4396.44	10.8395	10.82773	3854.91	4396.30	10.067
1000	58.75669	4053.01	4640.58	11.0392	11.75087	4052.91	4640.46	10.2964
1100	63.37198	4257.47	4891.19	11.2287	12.67418	4257.37	4891.08	10.4898
1200	67.98724	4467.93	5147.78	11.4086	13.59737	4467.82	5147.69	10.6682
1300	72.60250	4683.58	5409.79	11.5789	14.52054	4683.58	5409.61	10.8382
100 kPa (99.62 °C)								
200 kPa (120.23 °C)								
Sat.	1.69400	2506.06	2675.46	7.2093	0.88573	2529.49	2706.63	7.1271
150	1.80826	2582.75	2776.58	7.4323	0.95864	2576.87	2768.00	7.2795
200	2.17226	2658.05	2875.27	7.8342	1.08034	2654.59	2870.46	7.5089
250	2.48876	2733.73	2974.33	8.0332	1.19880	2731.22	2970.98	7.7085
300	2.63876	2810.41	3074.28	8.2157	1.31616	2808.55	3071.79	7.8936
400	3.10363	2967.85	3278.11	8.5434	1.54930	2966.09	3276.55	8.2217
500	3.56547	3131.54	3489.09	8.8341	1.79139	3130.73	3487.03	8.5132
600	4.02351	3301.94	3704.72	9.0975	2.03297	3301.36	3702.96	8.7789
700	4.48086	3479.24	3928.23	9.3388	2.24426	3478.81	3927.65	9.0194
800	4.93574	3663.53	4158.71	9.5652	2.47330	3663.19	4158.27	9.2430
900	5.41353	3854.77	4396.12	9.7787	2.70643	3854.49	4395.77	9.4561
1000	5.87526	4052.78	4640.31	9.9784	2.93740	4052.53	4640.01	9.6563
1100	6.32096	4257.25	4890.95	10.1658	3.16834	4257.91	4890.68	9.8458
1200	6.76863	4467.79	5147.56	10.3462	3.39927	4467.46	5147.32	10.0182
1300	7.20930	4683.47	5409.49	10.5182	3.63019	4682.71	5409.26	10.1802

[3] BORGNAKKE, C., SONNTAG, R. E., SOM, *Fundamental of Thermodynamics, Seventh Edition, Wiley Publication*

So, at 200 degree centigrade so this table will be continued up to even higher temperatures; so, at 200 degree centigrade you have to look what is v f and what is v g. So, at 200 degree centigrade you have so, I have the data with me, I can tell you at 200

degree centigrade this you can verify from the table saturated table v_f is 1.56 into 10 to the power 1.565 into 10 to the power minus 3 meter cube per kg and v_g is 0.12736.

This is from saturated table ok. Now, you tell your v is between v_f and v_g right. So, your v is 0.8 11 which is in between these two values. So, v_2 is between v_f and v_g at T_2 ; if that be the case then the state point 2 will lie somewhere here in the two phase region. So, what is the specific volume at state 2? It is same as v_1 . What is the quality at state 2? So, v_2 is $x v_g + (1 - x) v_f$, this formula has been derived earlier in one of the classes.

So, I will not get into the details here, but you see the point that I want to raise is that it is for this reason that we use specific volume not density. See the specific volume of the mixture is a weighted average of the specific volumes of the liquid and vapor phases, not the weighted average of the density right. So, by using law of mixture it is very easy to calculate the properties of mixtures. So, here x is what mass of vapor at state 2 by total mass. So, you have v_g and v_f this two and v_2 . So, from here you can calculate what is x ok. So, once you have calculated x .

So, you can check this should be between 0 and 1; that means, you have you are there in the two phase region. In the process 2 to 3 you have T_3 is equal to T_2 and p_3 is 2.5 MPa. So now, again you have to see at 200 degree centigrade or at 2.5 MPa whatever you look into the saturated table. So, let us let us see that at 2.5 MPa what is the saturation temperature; so, 2.5 MPa. So, let us look into the saturation temperature at 2.5 MPa. So, even in the superheated vapor tables the saturation temperature is indicated.

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Steam Table – Compressed Liquid Water _[4]									
Temp (°C)	v (m ³ /kg)	u (kJ/kg)	h (kJ/kg)	s (kJ/kg K)	v (m ³ /kg)	u (kJ/kg)	h (kJ/kg)	s (kJ/kg K)	
500 kPa (11.80 °C)					2000 kPa (212.42 °C)				
Sat.	0.001903	629.66	640.21	1.8606	0.001777	906.42	908.77	2.4473	
0	0.000999	0.02	0.51	0.0000	0.000999	0.03	2.03	0.0001	
20	0.001002	83.91	84.41	0.2955	0.001001	83.82	83.82	2.962	
40	0.001008	167.47	167.98	0.5722	0.001007	167.29	169.30	5.714	
60	0.001017	251.00	251.51	0.8308	0.001016	250.73	252.77	8.500	
80	0.001029	334.73	335.24	1.0749	0.001028	334.38	336.44	1.0739	
100	0.001043	418.80	419.32	1.3065	0.001043	418.36	420.45	1.3053	
120	0.001060	503.37	503.90	1.5273	0.001059	502.84	504.96	1.5259	
140	0.001080	588.66	589.20	1.7389	0.001079	588.02	590.18	1.7373	
160	—	—	—	—	0.001101	674.14	676.34	1.9410	
180	—	—	—	—	0.001127	761.46	763.71	2.1382	
200	—	—	—	—	0.001156	850.30	852.61	2.3301	
5000 kPa (263.99 °C)					10000 kPa (311.06 °C)				
Sat.	0.001286	1147.78	1154.21	2.8201	0.001452	1303.00	1407.53	3.3505	
0	0.000998	0.03	5.02	0.0001	0.000995	0.10	10.05	0.0003	
20	0.001000	83.64	88.64	0.2955	0.000997	83.35	93.32	0.2945	
40	0.001006	166.93	171.95	0.5795	0.001003	166.33	176.36	0.5685	
60	0.001015	250.21	255.28	0.8284	0.001013	249.34	259.47	0.8258	
80	0.001027	333.69	338.83	1.0719	0.001025	332.56	342.81	1.0687	
100	0.001041	417.50	422.71	1.3020	0.001039	416.60	426.88	1.2992	
120	0.001058	501.79	507.07	1.5225	0.001055	500.67	510.81	1.5188	
140	0.001077	586.74	592.13	1.7342	0.001074	584.67	594.80	1.7291	
160	0.001099	672.41	678.10	1.9374	0.001195	670.11	681.07	1.9338	
180	0.001124	759.62	765.24	2.1341	0.001120	756.63	767.83	2.1274	
200	0.001153	848.08	853.85	2.3254	0.001148	844.40	855.87	2.3178	
220	0.001187	938.43	944.36	2.5128	0.001181	934.07	945.88	2.5038	
240	0.001226	1031.34	1037.47	2.6978	0.001219	1025.94	1038.13	2.6872	
260	0.001275	1127.92	1134.30	2.8829	0.001265	1121.03	1133.68	2.8698	
280	—	—	—	—	0.001322	1220.90	1234.11	3.0547	
300	—	—	—	—	0.001397	1328.34	1342.31	3.2400	

[4] BORGNAKKE, C., SONNTAG, R. E., SOM, Fundamental of Thermodynamics, Seventh Edition, Wiley Publication.

So, 2.5 MPa is what? 2.5 MPa just look into the superheated water vapor table; so 2.5 MPa or 200 degree centigrade; let us say 200 degree centigrade. So, 200 degree centigrade I do not have the data at 200 degree centigrade. But, if you look into the 200 degree centigrade you will have the saturation temperature at 200 degree centigrade. If you will look into the property table I do not have that part of the table, but I have the data at 200 degree centigrade the saturation pressure is 1.553 MPa.

That part of the table I do not have at this moment, but this is your homework. So, I have deliberately left that part of the table out. So, I have only kept up to 100 degree centigrade which you see here, you will have an extension of this up to higher temperatures. So, at 100 degree centigrade the saturation pressure is 101.3 kilo Pascal. Similarly, from the saturation table at 200 degree centigrade you will get the saturation pressure as 1.553 mega Pascal. Now, this p_3 is greater than that; that means it is in a compressed liquid state. So, p_3 is greater than p_{sat} at T_3 , this means it is 3 in compressed liquid.

So, compress liquid in other case in other words is also called as sub cooled liquid. What does it mean? It means that at 2.5 mega Pascal whatever is the saturation temperature, this temperature is less than that saturation temperature. So, from that angle from the temperature angle you can call it sub cooled, from the pressure angle you can call it

compressed liquid all the same. So, at the state point 3 it will be in the fully liquid state and from 2 to 3, it will be something like this isothermal process.

So, 1 to 2 like this and 2 to 3 like this. So, how to identify state 3? 200 degree centigrade and p_3 as 2.5 MPa which table you should look for now. So, we have looked into the saturated water table and the superheated water vapor table; there is a third table which is called as compressed liquid water table. So, at 2.5 mega Pascal you see that you have a table at 2 mega Pascal and 5 mega Pascal. So, 2.5 you may have to interpolate, at 2 mega Pascal at 200 degree centigrade you have a specific volume.

So, I am using this part of the board at 2 mega Pascal 200 degree centigrade the specific volume is 0.001156 ok. Let us write it in 1 line 0.01156 and at 5 MPa see the table does not contain 2.5 MPa at 5 MPa 200 degree centigrade it is 0.001153 ok. So, the question is at 2.5 MPa what is that? So, let us say that at 2.5 MPa it is v_3 . So, v_3 minus 0.001153 by 0.01156 minus 0.001153 we are doing an interpolation.

It is v_3 is p_3 which is the corresponding pressure is p_3 equal to 2.5 minus the corresponding pressure is 5 divided by 2 minus 5 right; y minus y_1 by y_2 minus y_1 is equal to x minus x_1 by x_2 minus x_1 . We are interpolating the pressure versus volume data with y as volume and x as pressure. So, this will tell you what is v_3 . The answer to this is 0.001155 meter cube per kg. See it is not always necessary to go through this laborious process, when it is state 3 and the temperature is around this 200 like that. So, water at 200 degree centigrade liquid water, what will be its density. It will not be far from 1000 kg per meter cube right.

So, 1 by specific volume will be 1 by 1000 and it will be close to that. So, at least 0.01 sorry this is 0.00 0.00115 not 01. So 0, this is 0.00 all another 0 is there I have missed this ok. So, 0.001153 0; these are all another 0 will be there. So, this mistake you can common you can very easily detect because, water density it normally is 1000. So, 1 by 1000 is 0.001. So, another 0 will be there so, you see that only in the third, fourth, fifth decimal the values are changing.

So, for all practical purposes if you even do not look into the table, but just figure out that it is a compressed liquid, then you can easily say that compressed liquid means it is almost like the density of water under normal temperature. I mean with from normal temperature to 200 degree centigrade the density of water will not vary that much, if it is

liquid water ok. So, this problem I have spent a lot of time, but I have try to make sure that by looking into the tables how can you identify these state points.

And, I hope this was useful. From the next lecture onwards we will start looking into some more specific problems on properties of pure substances.

Thank you.