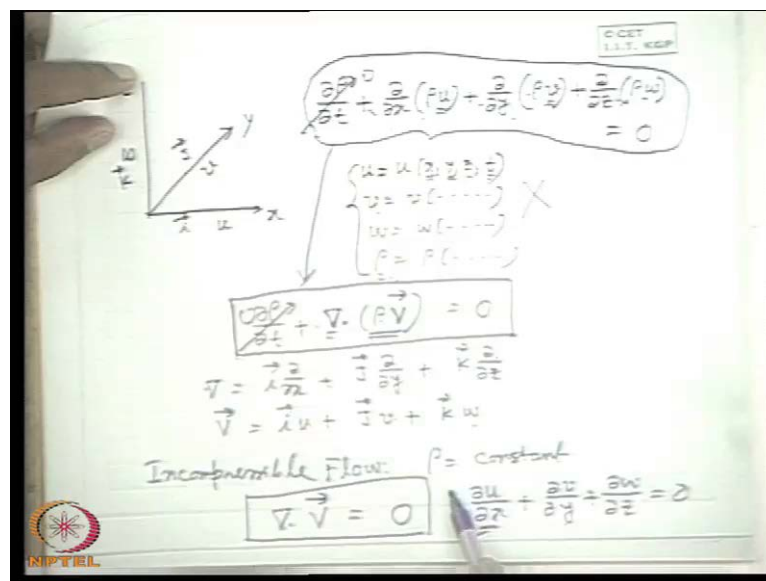


Fluid Mechanics
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Lecture - 14
Conservation Equations in Fluid Flow Part-II

Good morning. I welcome you all to this session. In last class, we were discussing, we have just started the discussion on continuity equation, and we derive the continuity equation in a Cartesian frame of reference. What is a continuity equation? If we recall, it is an equation relating to the velocity and density field in a flow of fluid, which is deduced from the principle of conservation of mass applied to a control volume that means, continuity equation basically signifies the principle of conservation of mass.

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Now, if we recall the equation, you please see here that in a Cartesian frame of reference, if you recall the equation, let this is the Cartesian frame that we discussed x, y, z. The equation of continuity was like this $\frac{\partial \rho}{\partial t} + \frac{\partial}{\partial x}(\rho u) + \frac{\partial}{\partial y}(\rho v) + \frac{\partial}{\partial z}(\rho w) = 0$. u is the x component velocity, v is the y component and w is the z component. So, typically this equation was derived from the principle of conservation of mass applied to a control volume with respect to a Cartesian coordinate system, rectangular Cartesian coordinate system. This is precisely the equations where ρ is the density and u v w are the velocity components.

Now, one thing we can tell from this equation. That in a flow field, if we get a description of u v w as a function of x y z and t as a function of x y z and t , v is also such functions of x y z and t , w is also such function of x y z and t and ρ is also such functions. That means, these dependent variables are hydrodynamic parameters. For example, three velocity components and density are expressed as a function of independent variables like the space coordinates and time. You know these are the independent variables.

Then, this function must satisfy this equation. Otherwise, the flow is impossible. Sometimes we check whether a velocity field and density field describe a physical flow or possible flow or not. If they do not satisfy this equation, means they do not satisfy the conservation of mass. That means, this is an impossible situation. This sets of functions can never represent the velocity field and density field of the fluid flow. It is most important for the use of continuity equation. You should know that.

Now, you see that this continuity equation can be defined or described with respect to different coordinate systems depending upon the geometry of the flow. Now, before doing that, we can just see that this equation expressed in Cartesian coordinate system can be written in a vector form like that, $\text{del } \rho \text{ del } t$ plus this term can be written as, if you recall your preliminary knowledge in vector, so, this term is divergence of $\rho \mathbf{v}$. ρ is a scalar and \mathbf{v} is a vector. So, $\rho \mathbf{v}$ is a vector.

You know the divergence operator is a vector operator, which is $\mathbf{i} \text{ del } \text{del } x$. For a Cartesian coordinate system, this tends like that. \mathbf{i} \mathbf{j} \mathbf{k} are the unit vector in x y and z direction. So, we can write the operator del , which is a vector operator \mathbf{k} , just if you brush up your preliminary knowledge in vector. So, this operator being used with a dot product, that is a scalar product with this vector, where \bar{v} that is the velocity field. You know this is a vector. So, this has got distinct three scalar components v and w along x y and z directions. So, if you multiply these two vectors, that is $\text{del} \cdot \rho \mathbf{v}$ dot scalar multiplication, we simply get this. So, that you know $\text{del } u \text{ del } x$ plus $\text{del } v \text{ del } y$ plus $\text{del } w \text{ del } z$.

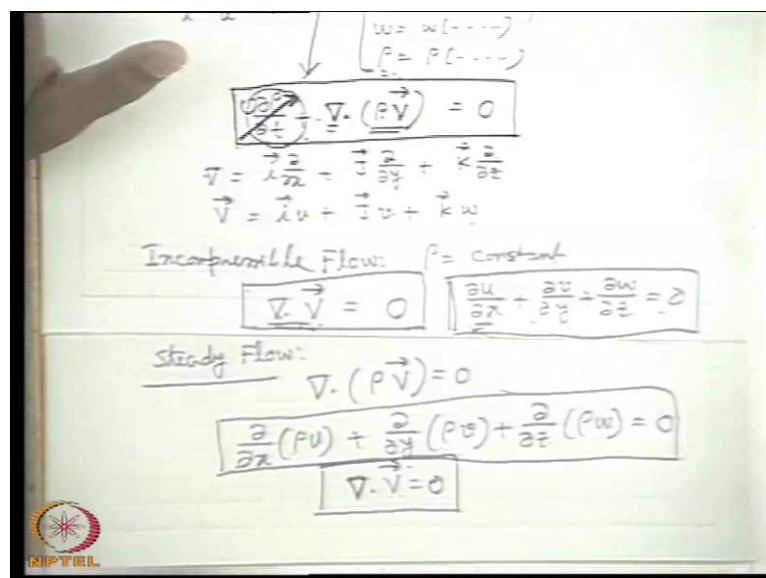
So therefore, one way of converting any equation from one coordinate system to other coordinate system is to see the equation in one coordinate system and to find out its vector form, general vector form. So, if you can do that, then we can tell that this is the

vector form and we can expand this vector form in different coordinate system. So that, we can get the equation in different coordinate system.

So, before coming to that, I should describe one thing, which probably we described earlier also. If the flow is incompressible, in the last class also, if the flow is incompressible means incompressible flow. If the flow is incompressible, rho is constant. That means, density does not change in the flow field neither with time nor with space coordinates. What does it mean that $\frac{d\rho}{dt} = 0$? That means, in this case, $\frac{d\rho}{dt}$ in this form $\frac{d\rho}{dt} = 0$.

Moreover, rho will come out from the differentials and in this operations, in this vector form rho will come out. So, ultimately the equations will be divergence of the velocity vector in vector form is 0. This is the equation of continuity for incompressible flow. In case of Cartesian coordinate, the expansion of this will be $\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z}$. That means, we can write this in vector form and then, expand in case of a Cartesian coordinate $\nabla \cdot \vec{v}$ will be $\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z}$. Because \vec{v} is a vector defined by like that and ∇ is the or we can straight forward get it from the equation with respect to Cartesian coordinate. That is will be 0 and rho will come out and the common factor which cannot be 0, so, $\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0$.

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This is the equation of continuity for incompressible flow. What will be the continuity equation for a steady flow? For a steady flow, please tell what is the continuity equation for a steady flow? Which term will be omitted for a steady flow? Steady flow means that parameters will not change with time. So, which term of these two terms $\frac{\partial \rho}{\partial t}$ will be 0? That means, for a steady flow, this is the equation of continuity. That means, in Cartesian coordinate, $\frac{\partial}{\partial x}(\rho u) + \frac{\partial}{\partial y}(\rho v)$ is a special case for a Cartesian coordinate system $\frac{\partial}{\partial z}(\rho w)$.

Now, one interesting fact you must remember that this is the continuity equation for a steady flow of both compressible and incompressible. So, if we take an additional constant of incompressible flow along with the steadiness, then ρ comes constant. Then, we get from either of the two equation divergence $\nabla \cdot \mathbf{v} = 0$. So, for a steady flow, this is the continuity equation. Now, for an incompressible flow you see the continuity equation is divergence $\nabla \cdot \mathbf{v} = 0$. So therefore, from an incompressible flow, continuity equation it is very difficult to infer whether the flow is steady or unsteady, because even if the flow is unsteady, but incompressible, the equation remains same which is the fact, what is the, why, what is the fact because the derivative of ρ with time only appears.

So, whenever the flow becomes incompressible, so, it automatically goes because ρ has to be constant for an incompressible flow. Even if it is unsteady, ρ cannot depend on time. Other parameters will depend on time. Since the time derivative of no other parameters appear in the continuity equation, therefore it is very difficult to judge from the continuity equation of an incompressible flow, whether the flow is steady or not. For example, whenever the flow is incompressible state becomes divergence $\nabla \cdot \mathbf{v} = 0$; and that means, this is 0.

So, even if the flow is steady, there is no scope of any further simplification or modification of this equation because time derivative of no variable appears in this equation. So therefore, the continuity equation for both steady and unsteady incompressible flow is given by divergence $\nabla \cdot \mathbf{v} = 0$. But for a compressible flow, there is a change between steady or unsteady equations in the form of continuity equation. This is why? Because this is the compressible unsteady flow and this is the compressible part. That means, the unsteady flow, compressible unsteady flow, a steady flow and this is the compressible unsteady flow.

So, a compressible flow, if it is unsteady, term will be there. If a compressible flow, if it is steady, then this term will not be there. So therefore, we can distinguish the steady flow or unsteady flow, if the flow is not incompressible from the continuity equation. But if the flow is incompressible, whether the flow is steady or unsteady, the continuity equation will always be divergence v is 0. This part is cleared?

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The image shows handwritten mathematical derivations on a whiteboard. On the left, a 3D coordinate system with x, y, and z axes is shown. A vector \vec{V} is drawn in the x-y plane, and its components V_x , V_y , and V_z are indicated. The magnitude of the vector is labeled as $|\vec{V}|$. To the right of the diagram, the following equations are written:

$$\nabla = \hat{i} \frac{\partial}{\partial x} + \hat{j} \frac{\partial}{\partial y} + \hat{k} \frac{\partial}{\partial z}$$

$$\nabla \cdot \vec{V} = \hat{i} \left(\frac{\partial}{\partial x} V_x \right) + \hat{j} \left(\frac{\partial}{\partial y} V_y \right) + \hat{k} \left(\frac{\partial}{\partial z} V_z \right)$$

$$\nabla \cdot \vec{V} = \frac{\partial}{\partial x} V_x + \frac{\partial}{\partial y} V_y + \frac{\partial}{\partial z} V_z$$

Below these, the continuity equation for a compressible fluid is derived:

$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \vec{V}) = 0$$

$$\frac{\partial \rho}{\partial t} + \frac{\partial}{\partial x} (\rho V_x) + \frac{\partial}{\partial y} (\rho V_y) + \frac{\partial}{\partial z} (\rho V_z) = 0$$

The bottom left corner of the whiteboard features the logo of NPTEL (National Programme on Technology Enhanced Learning).

Now, next I come to the different coordinate system. Now let us, first thing that is equation in general for a incompressible unsteady flow, this is the divergence of ρv . If the question comes, what is the cylindrical coordinate? What is the continuity equation in cylindrical coordinate system? Continuity equation in cylindrical coordinate system. So, one way, for example what is cylindrical coordinate system? Let us concentrate the cylindrical coordinate system. Let this x and this y and this z .

In a cylindrical coordinate system, instead of x, y , we define in x, y plane, the point by a radial location r and Azimuthal coordinate θ and the z will be same. That is, in the z direction, this has come from the concept of a cylinder, geometry of a cylinder. So that, at any point will be described by a radius radial vector or radial coordinate r azimuthal θ and this z . You know these things. That means, r, θ, z instead of x, y . These are the coordinates in a cylindrical polar coordinate system and not simply cylindrical coordinate system.

In that case, one way of, did you see it? Mathematically, without going for any other physical complications, simply expand this term. But before expanding this term, one has to know the mathematical expression for this ∇ in different coordinate system. Probably, you know, if we again brush up your preliminary knowledge in vector, this ∇ in Cartesian coordinate as I have written earlier, that represents $\nabla = i \frac{\partial}{\partial x} + j \frac{\partial}{\partial y} + k \frac{\partial}{\partial z}$, where i, j, k are the unit vector along x, y and z direction.

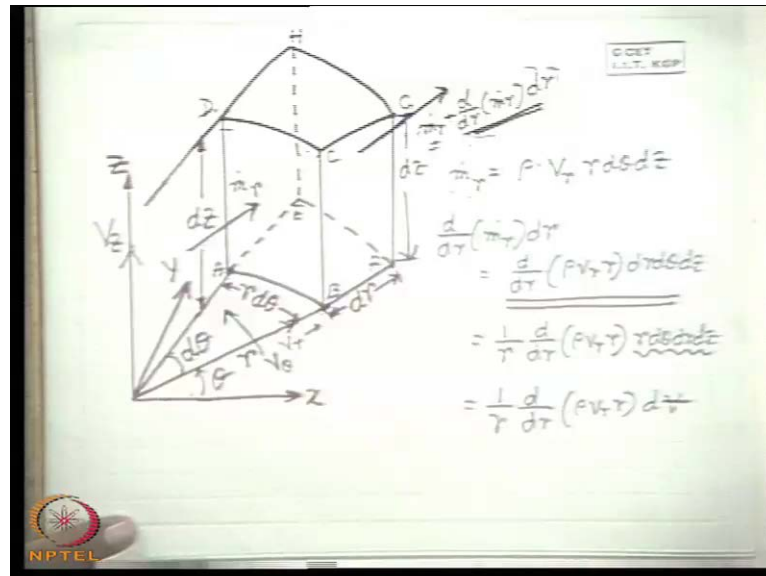
Similarly, in cylindrical coordinate system, this will be $\nabla = i \frac{\partial}{\partial r} + \frac{1}{r} \frac{\partial}{\partial \theta} + k \frac{\partial}{\partial z}$, where i, j, k at the unit vectors along r , along this θ direction j and along the z direction remains as it is. So, if you define i, j, k , the unit vectors along the coordinate directions r, θ and j , this is the operator. One knows this thing. For him, it is easy to find out $\nabla \cdot \rho v$ because v in Cartesian coordinate system, if you represent v in r, θ, z as the radial component of velocity and v_θ ; that means, this direction, the azimuthal direction is the v_θ tangential component of velocity or azimuthal component of velocity. v_z is the z component, which we are using w in case of Cartesian coordinate system.

Now, we are using v_z ; that means, the velocity field can be expressed as its components $v_\theta + k v_z$. So, one can find out now, after knowing this and these two velocity fields, ρ is a scalar function that divergence of ρv . Well, any questions please? So, this will be this multiplied with this, that means, $\nabla \cdot \rho v = \frac{\partial}{\partial r}(\rho v_r) + \frac{1}{r} \frac{\partial}{\partial \theta}(\rho v_\theta) + \frac{\partial}{\partial z}(\rho v_z)$. I am sorry. This will be multiplied with ρ . So, $\nabla \cdot \rho v = \frac{\partial}{\partial r}(\rho v_r) + \frac{1}{r} \frac{\partial}{\partial \theta}(\rho v_\theta) + \frac{\partial}{\partial z}(\rho v_z)$. Just simple mathematics. That means, what I do? I expand this term, this second term in a cylindrical polar coordinate or simply cylindrical coordinate system. If I do so, then I can write the continuity equation, another additional term; that means, is $\frac{\partial \rho}{\partial t} + \nabla \cdot \rho v = 0$. This is the general vector form.

That means, I have expanded this in cylindrical coordinate system. That means, therefore, I can tell precisely this is the continuity equation in cylindrical coordinate system, where v_r, v_θ, v_z are the respective velocity components corresponding to that coordinate system. So, this is one way of reducing the continuity equation in different coordinate system. We can do it for spherical coordinate system also. That I left

as an exercise to you. By expanding this term, this is a purely mathematical exercise. But one can again find out these from physical concept or from fundamentals.

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What I told in the last class is that, if we have to derive the continuity equation from the fundamentals, means application of conservation equation to a control volume, then the first term is that, you will have to take the control volume appropriate to a coordinate system. Now, look into this figure. Now, if we want to derive the continuity equation in a cylindrical polar coordinate system, which is defined by a radial location R azimuthal, this is the azimuthal θ and Z , then we will have to consider as volume, which is parallel in case of a Cartesian coordinate system. Now, the control volume will be like this, where the different planes of the control volume will be parallel to the coordinate planes.

So, how we will choose it? This one direction will be $r d\theta$. If this is r and this radius vector is at an angle $d\theta$, so, this angle is $d\theta$. Another length will be dr and this will be definitely dz . That means, a control volume of dimensions $dr d\theta r d\theta dz$, this type of a fluid element or a slice of a fluid element have to be considered. Now, let us give some name, otherwise it is difficult to $A B C D$ and this one is $E F G H$. Now, $A B C D E F G H$ represents the control volume.

Now, you see we have to represent the mass flux in different directions. So, there is velocity in r direction. So therefore, there is a mass influx. Now, let us consider, due to

the r direction velocity v_r , so, velocities are in r direction, theta direction v_θ , this is the v_θ , theta direction, this is the v_r in r direction. This is as usual v_z . Here, we represent v_z not as w , v_z direction velocity.

Now, if we concentrate in the similar fashion, the mass flux in the radial direction which is across the surface $A B C D$. This is $A B C D$. That means, the r surface which is perpendicular to the radial direction. So mass influx, if we consider as $m \cdot r$ and the mass efflux from the r plane; that means, this plane $E F G H$, there are two r planes; that means, planes perpendicular to radial direction. One is $A B C D$ and another is $E F G H$.

So, because of the existence of the velocity vector, we are in its usual positive direction. Mass will come into the control volume across $A B C D$ surface and mass will leave the control volume across $E F G H$ surface. So, this will be $m \cdot r$ plus $d \cdot r$ of $m \cdot r \cdot d r$ because this mass flux has changed by this amount because of a change in $d r$. In similar fashion, we write what is the expression of $m \cdot r$, that is the mass flux across this surface. It is the volume flux times the area. So, volume flux will be density. Sorry, density will come for the mass. Let us write the volume flux will be the velocity times the area. What is the area of this surface $r \cdot d \theta$ and $d z$? That means, already I get this $d z$. Again it is duplication. Does not matter $r \cdot d \theta \cdot d z$ and ρ is multiplied to keep $m \cdot r$. So therefore, what is this $m \cdot r \cdot d r \cdot m \cdot r \cdot d r$? That means, let us write it only $d r \cdot m \cdot r \cdot d r$. This will be equal to $d \cdot r$ of $\rho \cdot v_r \cdot r$. So, $d r \cdot d \theta \cdot d z$, I take out.

Now, you see the net mass efflux. Because of the mass flux across the r surfaces or r planes; that means, the plane perpendicular to r , because of these two planes $A B C D$ and $E F G H$ is this minus this. So, net mass efflux, I am not writing. I just tell you net mass efflux from the control volume. Because of the mass flux is across the r planes, that is planes perpendicular to r direction; that means, these two planes $A B C D E F G H$ is equal to this minus this. That means, $m \cdot d \cdot r$ of $m \cdot d \cdot r$. That means this quantity. This is the net mass efflux, because of the flux across the r planes.

This we can write by taking 1 by r multiply and then v_r , little rearrangement $d \theta \cdot d r \cdot d z$. What is $r \cdot d \theta \cdot d r \cdot d z$? Volume. Very good. So, 1 by $r \cdot d \cdot r$ of $\rho \cdot v_r \cdot r$ into $d \cdot v$. In the similar way, we can find out for mass fluxes across the theta.

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Handwritten derivation on a whiteboard:

$$m = \rho V = \rho r dr dz$$

$$\frac{d}{dt}(m) dz = \frac{\partial}{\partial t}(\rho r dr dz) dz$$

$$= \frac{1}{r} \frac{\partial}{\partial t}(\rho r) dr dz$$

Net mass efflux from C.V.

$$= \left\{ \frac{1}{r} \frac{\partial}{\partial t}(\rho r) + \frac{1}{r} \frac{\partial}{\partial r}(\rho r v_r) \right\} dr dz$$

$$= \frac{\partial}{\partial t}(\rho r dr dz) + \frac{\partial}{\partial r}(\rho r v_r dr dz)$$

Continuity equation

$$\frac{\partial}{\partial t}(\rho r dr dz) + \frac{\partial}{\partial r}(\rho r v_r dr dz) = 0$$

$$\frac{\partial}{\partial t} + \frac{\partial}{\partial r} \left[\rho r v_r \right] = 0$$

That means, $m \cdot \theta$. That means, θ direction. That means, the mass flux due to the planes perpendicular to θ directions; that means, now we are interested for mass flux across the planes B F G H and A E H D. Two parallel θ planes perpendicular to θ direction.

Now, because of the existence of the v_r which is the component of the velocity in its usual positive direction, the mass flux will enter the control volume across B F G H. Let us define that $m \cdot \theta$. Because of the same reason, the mass flux will go out of the control volume across this plane or phase A E H D, which we should write $m \cdot \theta$. Why because this is change at this location, because of a change in $r \cdot \theta$.

So, you can write in terms of $d\theta$, $d \cdot d\theta$ because in the θ direction, angular direction we are doing it $m \cdot \theta \cdot d\theta$. So, what is $m \cdot \theta$? Please tell me. $m \cdot \theta$ now, we will be mass into the volume flow, that is v_θ times the dr into dz . Very good. dr into dz . All right. Now, what will be this $m \cdot d\theta$ of $m \cdot \theta \cdot d\theta$? This will be equal to $\frac{\partial}{\partial \theta}(\rho r v_\theta) dr dz d\theta$. So, this can be written as $\frac{1}{r} \frac{\partial}{\partial \theta}(\rho r v_\theta) dr dz d\theta$. That means, this is dV , where dV is the elemental volume of this control volume. Again, this is the quantity which represents the net mass efflux from the control volume due to the mass fluxes across these two planes. That is θ planes B F G C and A E H D.

So, this represents simply the net mass flux, from the mass efflux, from the control volume due to the mass flux across these two parallel planes. That is, the planes perpendicular to theta direction. Similar way, if we see or if we investigate the mass fluxes through planes perpendicular to z direction. What are the planes? A B F E and D C G H. That means, bottom and top plane in this drawing.

So, due to the existence of the positive direction velocity v_z , in usual positive direction of the coordinate axis, the mass will come into the control volume across the phase A B F E. Similarly, the mass will leave the control volume across the phase D C G H. Simply we can write now ρ , this will be v_z times $r \, d\theta \, dr$. Simply this will be $m \cdot z$ plus $d \, dz$ of $m \cdot z \, dz$ as usual. That means, there is a change in the mass flow because of a vertical displacement of dz . So, $d \, dz$ of $m \cdot z \, dz$ can be written as, rather I can write $d \, dz$ that is $\partial \partial z$. I am writing in this fashion though I am writing $d \, dz$, but ultimately this is a partial differential. That is why I am changing from d to ∂ . Does not matter.

So, this will be equal to $\partial \partial z$. You can write all these in terms of ∂ , because in the conception there is no problem. But in a mathematical notation, this is not a total differential concept because these are all partial differential. Because all the quantities vary with both $r \, \theta \, z$ and time also. So, this is an instantaneous picture. So that, when we make differentiation with j this should be ∂ only.

However, for the conception there is no problem. So, $\partial \partial z$ of what we can $(()) \rho \, v_z$ and $r \, d\theta \, dr \, dz$ will automatically make $d \, v$. This is nothing but the amount, which corresponds to the net efflux to the control volume due to the fluxes is across the z planes. That means, across two planes A B A V and D C G H. So therefore, we get this is the net efflux from the control volume due to the mass fluxes across r planes. Similarly, this is the net efflux from the control volume due to the mass fluxes across theta planes and this is the mass efflux from the control volume due to mass fluxes across z plane.

So, net mass efflux from the control volume will be sum of this. That means, $\partial \partial r$, if you want to have a look, 1 upon $r \, \partial \partial r \, \rho \, v_r$. So, I now write with this 1 by $r \, \partial \partial r \, \rho \, v_r$ into r . You can have a look; plus $d \, v$, we will take common, plus this 1 by $r \, \partial \partial \theta$ of $\rho \, v_\theta$ plus $\partial \partial z$ of $\rho \, v_z$ into $d \, v$ plus. If you recall this is the net mass efflux. So, continuity equation will be what? Continuity equation therefore, if you

recall the continuity equation in its statement form that the net rate of mass efflux from the control volume plus the rate of change of mass within the control volume.

So control volume, volume is dV and ρ is its density. So, it is the instantaneous mass within the control volume. So, rate of change of mass within the control volume will be $\frac{d}{dt}(\rho dV)$ plus this quantity. That means, I am not writing it again dV is equal to 0. That means this quantity. So, dV will come out of this $\frac{d}{dt}$ because control volume by definition and dV is fixed. So therefore, we can write $\frac{d}{dt}$ plus, this in bracket; that means, this term, the entire thing dV is equal to 0. dV cannot be 0. It is valid for any volume, any finite volume of the control volume. So, this part will be 0.

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The image shows a handwritten derivation of the continuity equation in cylindrical coordinates. The top equation is enclosed in a box and reads:
$$\frac{\partial \rho}{\partial t} + \frac{1}{r} \frac{\partial}{\partial r} (\rho v_r r) + \frac{1}{r} \frac{\partial}{\partial \theta} (\rho v_\theta r) + \frac{\partial}{\partial z} (\rho v_z) = 0$$
The bottom equation is underlined and reads:
$$\frac{\partial \rho}{\partial t} + \frac{\partial}{\partial r} (\rho v_r) + \frac{v_r}{r} + \frac{1}{r} \frac{\partial}{\partial \theta} (\rho v_\theta) + \frac{\partial}{\partial z} (\rho v_z) = 0$$
A small logo for 'CCET U.T. KGP' is visible in the top right corner of the slide, and a 'NPTEL' logo is in the bottom left corner.

So therefore, in the similar fashion, we can write that finally, $\frac{d\rho}{dt}$ plus, now I write $\frac{1}{r} \frac{d}{dr}(\rho v_r r)$ into $\frac{d}{dr}(\rho v_r) + \frac{v_r}{r}$ plus this probably. You can see that this I am writing $\frac{1}{r} \frac{d}{d\theta}(\rho v_\theta r)$ plus $\frac{d}{dz}(\rho v_z)$ is equal to 0. So, this is the precisely the continuity equation. We can write it in a different form, $\frac{d\rho}{dt}$. If we just expand this, the differentiation $\frac{d}{dr}(\rho v_r r)$, so we can get we can write $\frac{d}{dr}(\rho v_r r)$ plus ρv_r by r , by taking ρv_r the first function, and r is the second function. If we differentiate it, this cooled level thing, $\frac{d}{d\theta}(\rho v_\theta r)$ plus.

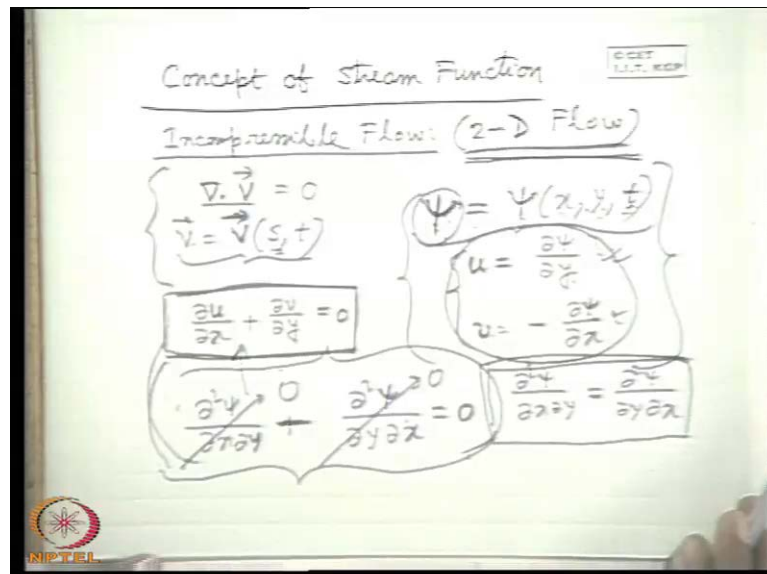
So, this is the equation we also derive straight from expanding the vector form of the continuity equation. So, there is no need always of deriving it from the fundamental. Just

for your conception, I show you. Because earlier, what we did was we know this vector form of the continuity equation. We simply expand this with the idea or with the knowledge that the del operator is defined in a cylindrical coordinate system like this, so that, we can straight away this in different coordinate systems.

For example, the expression in Cartesian coordinate system will be $\text{del del } x \text{ of } \rho u$ plus $\text{del del } y \text{ of } \rho v$ plus $\text{del del } z \text{ of } \rho w$. Similarly, for a cylindrical coordinate system, this will be the expression. But this can also be derived again from the fundamental. That means, taking a control volume appropriate to a coordinate system. For example, they are cylindrical coordinate system and applying the law of conservation of mass, considering all the mass fluxes coming in and coming out from the control volume across different plane surfaces, so that, I can or we can derive the continuity equation.

Similar way, the continuity equation can be derived in a spherical coordinate system. Again we will make more complications, because the control volume will be little complicated by geometry either by using the fundamental concept or by expanding these forms, which is left as an exercise to you.

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Now after this, I will go to a very important concept in a fluid flow, which is the concept of stream function. What is a stream function, concept of stream function? Now, we know that for an incompressible steady flow or we should not always tell that is

incompressible steady even for an incompressible flow. That means, even if it is steady or unsteady, the continuity equation is such that, means, if $(\nabla \cdot \mathbf{v}) = 0$ I have an incompressible flow. My velocity fields are given as a function of space coordinates and t , with scalar components u as a function of x, y, z, t , v as a function of, if it is a Cartesian coordinate system. Or, if it is a cylindrical coordinate, it will be a function of r, θ, z, t . So, I am just describing in generally one test and claims, that is flow is incompressible one can tell him. Please wait. I will check whether your velocity functions explicitly given in this form satisfies this particular equation or not. Divergence of $\mathbf{v} = 0$, if it is satisfied, we will tell your flow field is possible. If it does not satisfied, then we can tell it is an erroneous flow field. This velocity function can never define an incompressible flow.

This is the concept. So therefore, if we come again to mathematics, the divergence of the velocity vector is 0 for an incompressible flow. Let us consider a Cartesian system. First, simply it is nothing but $\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$. Always we consider a two dimensional flow stream. Concept of stream function is associated only for a two dimensional flow. You must know, this is not for a three dimensional flow. In three dimensional asymmetric flow only, which again reduces the three dimensional flow in a two dimensional flow. I will explain it afterwards. Then, we can define this stream function. Usually the stream function is defined only for two dimensional flow.

So, for a two dimensional flow, the expansion of this term for a Cartesian coordinate system is like that. Or in other words, in a two dimensional flow, defining u and v as a function of x, y and t , the continuity equation for an incompressible flow at any instant is this. Now, if I define a function ψ , which is a function of x, y and t , at any instant t . If it is an unsteady flow, the variable t will come. Otherwise, it will be a function of x and y only. That means, if in a two dimensional flow field, I defined a function. Think mathematically first. I defined a function, so that these functions satisfies this condition u is equal to $\frac{\partial \psi}{\partial y}$ and v is equal to minus $\frac{\partial \psi}{\partial x}$. That means this function is such whose partial derivative with respect to y , defines the x component of velocity at a particular point. If it is a function of time, this will be a function of time also. Similarly, its x derivative with respect to x with a negative sign defines the velocity, y component velocity at that instant and then, this function is defined as the stream function.

Now, question comes, why so arbitrarily we are defining a function such that u becomes $\frac{\partial \psi}{\partial y}$ and v becomes minus $\frac{\partial \psi}{\partial x}$. Mathematically it is understandable. We

will define a function ψ , which is a function of x , y and t in such a way, that u and v are defined in terms of this function in this manner. Then, this function is called this stream function. But what is the significance of it?

Let us now see the mathematical significance. If you defined this way, then if we put this stream function in continuity equation; that means, if the continuity equation is now substituted in terms of the stream function, what we will get first term? $\nabla^2 \psi$. What we will get in the next term? It is minus $\nabla^2 \psi$. Now, if ψ is a continuous function of x and y , you know that this order change does not have any difference. That means, $\nabla^2 \psi$ is $\nabla^2 \psi$. That means, if you differentiate ψ first, we take and then with y or first with y and then with x , they will be equal if the function is continuous.

Again brushing up your school level mathematics. So therefore, this is equal to 0. That means, it is automatically satisfied. That means, we do not get any extra equation as a continuity equation, if the flow field is defined in terms of stream function. Try to understand. This is a real tough concept. This level, only by reading books you may not understand this. That means, instead of defining flow field in terms of u , v , if we define a flow field in terms of stream function, it automatically satisfies the continuity equation. Because if we substitute the stream function, because stream function is defined this way.

So that, if we substitute this continuity equation get 0; that means, if we define this flow field in terms of a stream function, so, continuity equation is automatically satisfied. That means, we do not have an extra equation to satisfy the conservation of mass; that means, the equation is automatically satisfied. This is the mathematical implication of stream function.

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The image shows a hand-drawn derivation on a whiteboard. At the top, the total differential of the stream function ψ is given as $d\psi = \frac{\partial\psi}{\partial t} dt + \frac{\partial\psi}{\partial x} dx + \frac{\partial\psi}{\partial y} dy$. Below this, it is simplified to $d\psi = \frac{\partial\psi}{\partial x} dx + \frac{\partial\psi}{\partial y} dy$. The velocity components are defined as $u = \frac{\partial\psi}{\partial y}$ and $v = -\frac{\partial\psi}{\partial x}$. These are substituted into the differential equation to yield $-v dx + u dy = 0$. This is identified as the "Equation of a streamline". Finally, the equation is rearranged to $\frac{dy}{dx} = \frac{v}{u}$ and boxed as $v dx - u dy = 0$. An arrow points from the boxed equation back to the streamline equation. An NPTEL logo is visible in the bottom left corner.

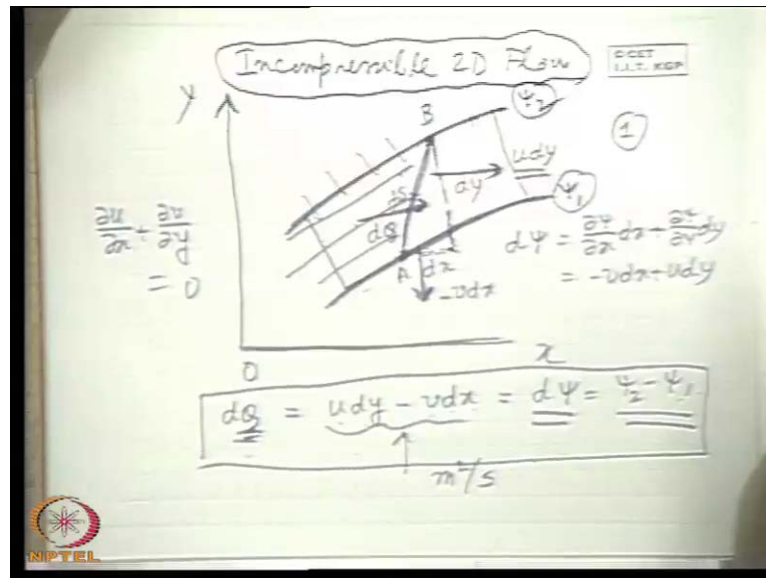
Let us see the physical implications of stream function. Now, before recognizing the physical implications of stream function, let us consider one thing that stream function is a function describing ψ as a function of x y . Now, a change in stream function. One interesting thing now we like to express. Now, we write a total change in stream function x y t . It can be written in mathematical form $\frac{\partial\psi}{\partial t} dt + \frac{\partial\psi}{\partial x} dx + \frac{\partial\psi}{\partial y} dy$ in a two dimensional flow.

Now, at any instant if you are interested that any instant value or for a steady flow, this term is not coming into picture. So therefore, $d\psi$ is equal to; that means, the change in the stream function at any instant or in a simplified manner, we can think of a steady flow, where the change in the stream function can be defined like this. It is very simple. It is no way connected to mechanic fluid. If there is a function of x y , the change in the functions ψ $d\psi$ is the change due to x and change due to y , $\frac{\partial\psi}{\partial x} dx + \frac{\partial\psi}{\partial y} dy$.

Now, what is the definition of stream function? This function is not a very arbitrary function. This is such a function that u is equal to $\frac{\partial\psi}{\partial y}$ or simply $\frac{\partial\psi}{\partial y}$ is equal to u and v is equal to minus $\frac{\partial\psi}{\partial x}$. So therefore, here I can write minus $v dx + u dy$. What is the value? Can you tell me along a streamline? Along a stream line, what is the value of right-hand side? For a streamline, the equation of streamline we know. What is the equation of a streamline? If you recollect, it is $\frac{dy}{dx} = \frac{v}{u}$

because the tangent at that line, at any point is the direction of the velocity vector. For a two dimensional case, streamline is $dy dx - v by u$. So therefore, $v dx - u dy$ or $u dx - v dy$ or $u dy - v dx$ is 0 along a streamline.

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So therefore, along a streamline, if this is a streamline this value is 0, which means, $d\psi$ is equal to 0 along a streamline. That means, the ψ function along a streamline, let us consider this is the x , this is the y , this is the z and this is a streamline. So, z concept does not come. It is only $x y$ concept. Let it is like this and there is x and y and this is a streamline. So, ψ functions, this is a streamline and this is a streamline. So, what we get? Along a streamline, the values of ψ are same. That means, ψ is equal to constant along a streamline. So, this is proved.

So, this is one of the very important conclusions that along a streamline $d\psi$ is 0; that means, ψ is equal to constant. So, ψ is equal to constant along a streamline. So therefore, in a two dimensional flow field, we can define streamlines by telling different values of ψ ; ψ_1 , ψ_2 , ψ_3 and ψ_4 , which are the constant values because ψ is constant along a streamline. It does not change along a streamline.

So, a streamline can be specified by giving a constant value of ψ stream function. From this, we can proceed another step further regarding the streamline, physical implication of streamline. Let us consider again $x y$, the two dimension and let us consider two ψ_1 and ψ_2 , the two streamlines, ψ_1 and ψ_2 . Let us consider one point A on a

streamline, any other point A and B on two streamline. Let us join. Now, let us make; Let us consider a control volume, whose dimension in this direction perpendicular to this plane of the figure or plane of the paper is unit. Let it be one unit and this length be ds , that is the length joining two points on two streamlines defined by stream functions ψ_1 and ψ_2 .

Therefore, this length, this is dy and this is dx obviously. Now, let us consider the flow field is such that because of which there is a flow coming into this control volume across this surface of length ds and plane unit dimension in this direction. If there is a flow coming into the control volume and if we consider the flow going out from these two planes, then what is the flow coming out from this? It is $u dy$ volume flow. Now, I have told that this concept of stream function, we are discussing for an incompressible 2D flow. It is always valid; incompressible 2D flow. Because from the very beginning, we have defined that the continuity equation, which is getting satisfied is $\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$. That means, basically it is two dimensional and incompressible.

So, in case of incompressible flow, the volume flow rate instead of mass product, we can use because ρ becomes a constant scale factor. That means, the volume flow which is coming to the control volume across these planes must go out from these two planes. If we consider through these two planes, the volume the fluid is going out. So, this is the volume flow rate across this phase and this is the volume flow rate across this phase because the area of this phase is dy into unit distance and area of this phase is dx into this distance unit. So therefore, we can write the dQ . If I tell the dQ amount of volume flow, q is the nomenclature for volume flow rate is crossing these planes, joining a and b must be equal to $u dy$. Now, this $v dx$ in this frame of reference, where y is positive in this way, then this will be minus $v dx$ because v is always negative sign. So, minus $v dx$ plus of minus $v dx$; that means, $u dy - v dx$.

Now, what is $u dy - v dx$? This is the difference $d\psi$ between the two points because if I relate $\psi_2 - \psi_1$ as $d\psi$, it will be $\frac{\partial \psi}{\partial x} dx + \frac{\partial \psi}{\partial y} dy$. That means, $u dx - v dy$. That means, this quantity, this is equal to $d\psi$; that means, this gives the difference of stream function between these two streamlines. So, this is the flow rate by unit length in the perpendicular direction. So, this gives the most important physical conclusion, that the difference in stream function between two adjacent streamlines, between two any

streamline gives the volume flow rate within the streamlines per unit in the normal direction.

There is no volume flow rate across a streamline. That means, if we consider a control volume like that, the volume is flowing like this. So, this is given. So, if we consider two streamlines and this consists of a stream tube; that means, bounded by two streamlines, then we can tell the volume flow through this channel made by two streamlines is given by the difference of these stream functions defining these two streamlines, per unit length or per unit width in the normal direction. Because if you see the unit, you see that $\psi_2 - \psi_1$ divided by $dy - dx$, this unit is meter square per second. That means, this is the volume flow rate per unit within this direction.

So, it is cleared. Therefore, we can tell that this stream function signifies this physical role that difference between this stream function gives the flow rate within the two streamlines. Well, I think we can conclude here. So, streamlines is like stream function is constant along a streamline. Stream function is a function of x and y , such a way that its derivative with respect to x and y coordinate, defines the velocity component in such a way that it automatically satisfies the equation of continuity and incompressible two dimensional flow. This is number one. Number two is the stream function remains constant along a streamline. Number three is the difference between the stream functions between two streamlines gives the rate of flow through these two streamlines along the channel found by two streamlines per unit width or length in the perpendicular direction.

Thank you.