

Viscous Fluid Flow
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Module - 12
Turbulent Flows - II
Lecture - 03
Turbulence Modelling

Hello everyone. So, you know that we have already derived the Reynolds averaged Navier-Stokes equations and there we have unknown Reynolds stress and later we used Boussinesq eddy viscosity approximation and we have written the apparent viscosity and summation of molecular viscosity plus turbulent viscosity.

Now, the question is how to model this turbulent viscosity μ_t ? For that today we will discuss few turbulence model and we will see how to find this μ_t .

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Turbulence Modelling

Reynolds Averaged Navier-Stokes Equation:

$$\rho \left(\frac{\partial \bar{u}_i}{\partial t} + \frac{\partial \bar{u}_i \bar{u}_j}{\partial x_j} \right) = -\frac{\partial \bar{p}}{\partial x_i} + \frac{\partial}{\partial x_j} \left(\mu \frac{\partial \bar{u}_i}{\partial x_j} - \rho \overline{u_i' u_j'} \right)$$

Using Boussinesq eddy viscosity approximation

$$\rho \left(\frac{\partial \bar{u}_i}{\partial t} + \frac{\partial \bar{u}_i \bar{u}_j}{\partial x_j} \right) = -\frac{\partial \bar{p}_{eff}}{\partial x_i} + \mu_{eff} \left(\frac{\partial \bar{u}_i}{\partial x_j} + \frac{\partial \bar{u}_j}{\partial x_i} \right)$$
$$\bar{p}_{eff} = \bar{p} + \frac{2}{3} \rho k \quad \mu_{eff} = \mu + \mu_t \quad \mu_t - \text{eddy viscosity}$$

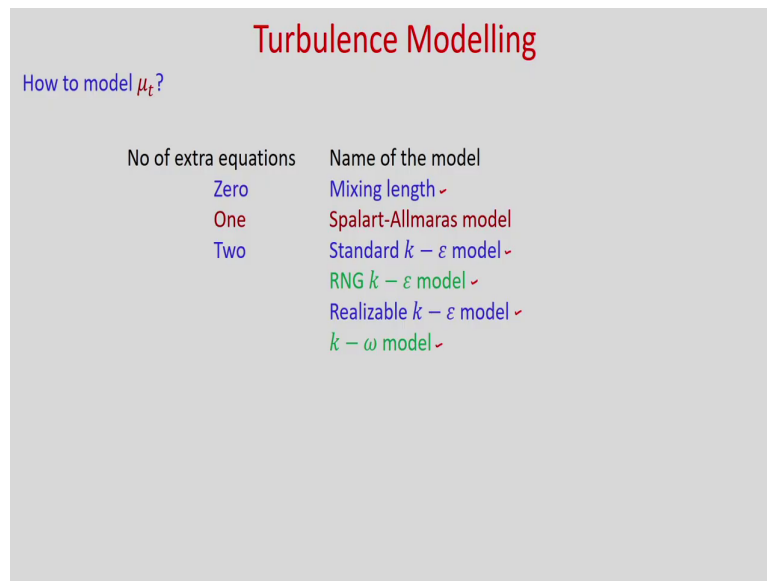
Turbulent kinetic energy:

$$k = \frac{1}{2} (\overline{u'^2} + \overline{v'^2} + \overline{w'^2})$$

So, you can see this is the Reynolds averaged Navier-Stokes equations we derived and this is the additional term Reynolds stress.

And then we used Boussinesq eddy viscosity approximation and we have written this equation, where this mu effective is mu plus mu t where mu t is eddy viscosity and it is still unknown. And this is the effective pressure, this is the mean pressure plus $\frac{2}{3} \rho k$, where k is the turbulent kinetic energy from this fluctuating velocity.

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| No of extra equations | Name of the model |
|-----------------------|-----------------------------------|
| Zero | Mixing length ✓ |
| One | Spalart-Allmaras model |
| Two | Standard $k - \epsilon$ model ✓ |
| | RNG $k - \epsilon$ model ✓ |
| | Realizable $k - \epsilon$ model ✓ |
| | $k - \omega$ model ✓ |

So, now how to determine this eddy viscosity? So, you can see that there are different models available. Already, we have discussed this Prandtl's mixing length hypothesis, where we do not need to solve any extra equation. So, that is a zero equation model. We have Spalart-Allmaras model, where we need to solve one extra equation and several two equation models are available like standard k epsilon, RNG k epsilon, Realizable k epsilon and k omega model.

So, if we want to model this turbulent flow numerically, then we need to solve these Reynolds averaged Navier-Stokes equations along with we need to solve some other equation to find the unknown eddy viscosity μ_t .

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Turbulence Modelling

Zero equation model: Mixing length

$$\underline{\mu}_t = \rho l^2 \left| \frac{\partial \bar{u}}{\partial y} \right|$$

Prandtl proposed the following model for the mixing length: $l = \underline{\kappa} y$

Leading to Prandtl's mixing-length model: $\underline{\mu}_t = \rho \kappa^2 y^2 \left| \frac{\partial \bar{u}}{\partial y} \right|$

You have seen that in zero equation model we just model this turbulent viscosity as rho l square, the absolute values of del u bar by del y, where l is the mixing length. So, you model this l using this Prandtl mixing length hypothesis as l is equal to kappa y.

So, you can see it is the simplest way to model it and if you use it then this turbulent viscosity you can write rho kappa square y square this absolute value of del u bar by del y, and you know that this is the absolute value we are taking such that the value of this turbulent viscosity will be positive.

So, you can see that it has advantages as it is easy to implement and it is computationally cheaper as you do not need to solve any additional equations to calculate these turbulent

viscosity. But, it has disadvantages like it is completely incapable of describing the flows with separation or circulation.

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Turbulence Modelling

Standard $k - \epsilon$ model

Turbulent kinetic energy:

$$k = \frac{1}{2} (\overline{u'^2} + \overline{v'^2} + \overline{w'^2})$$

Dissipation rate of k :

$$\epsilon = \nu \overline{\frac{\partial u'_i}{\partial x_j} \frac{\partial u'_i}{\partial x_j}}$$

Now, let us discuss one of the two equation turbulence model. So, we will first discuss about the standard k epsilon model. So, you can see k stands for turbulent kinetic energy and this epsilon is the dissipation rate of this turbulent kinetic energy. So, epsilon generally is represented as $\nu \overline{\frac{\partial u'_i}{\partial x_j} \frac{\partial u'_i}{\partial x_j}}$ and time average.

So, now, let us derive the equation for this turbulent kinetic energy and then we will write down the equation for this dissipation rate epsilon.

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Turbulence Modelling

$$\frac{\partial u_i}{\partial t} + \frac{\partial}{\partial x_j} (u_i u_j) = -\frac{1}{\rho} \frac{\partial p}{\partial x_i} + \nu \frac{\partial^2 u_i}{\partial x_j^2} \dots (1)$$

$u_i = \bar{u}_i + u_i', \quad u_j = \bar{u}_j + u_j', \quad p = \bar{p} + p'$

$$\frac{\partial \bar{u}_i}{\partial t} + \frac{\partial \bar{u}_i'}{\partial t} + \frac{\partial}{\partial x_j} (\bar{u}_i \bar{u}_j + \bar{u}_i' u_j' + \bar{u}_i u_j' + u_i' \bar{u}_j)$$

$$= -\frac{1}{\rho} \frac{\partial \bar{p}}{\partial x_i} - \frac{1}{\rho} \frac{\partial p'}{\partial x_j} + \nu \frac{\partial^2 \bar{u}_i}{\partial x_j^2} + \nu \frac{\partial^2 u_i'}{\partial x_j^2}$$

$$\frac{\partial \bar{u}_i}{\partial t} + \frac{\partial}{\partial x_j} (\bar{u}_i \bar{u}_j + \overline{u_i' u_j'}) = -\frac{1}{\rho} \frac{\partial \bar{p}}{\partial x_i} + \nu \frac{\partial^2 \bar{u}_i}{\partial x_j^2} \dots (2)$$

$$\frac{\partial \bar{u}_i}{\partial t} + \frac{\partial}{\partial x_j} (\bar{u}_i \bar{u}_j) = -\frac{1}{\rho} \frac{\partial \bar{p}}{\partial x_i} + \nu \frac{\partial^2 \bar{u}_i}{\partial x_j^2} - \frac{\partial}{\partial x_j} (\overline{u_i' u_j'}) \dots (3)$$

Subtract Eq. (2) from Eq. (1)

$$\frac{\partial u_i'}{\partial t} + \frac{\partial}{\partial x_j} (\bar{u}_i u_j' + \bar{u}_j u_i' + u_i' u_j' - \overline{u_i' u_j'}) = -\frac{1}{\rho} \frac{\partial p'}{\partial x_i} + \nu \frac{\partial^2 u_i'}{\partial x_j^2} \dots (3)$$

Multiply Eq. (2) by u_i'

$$u_i' \frac{\partial u_i'}{\partial t} + u_i' \frac{\partial}{\partial x_j} (\bar{u}_i u_j' + \bar{u}_j u_i' + u_i' u_j' - \overline{u_i' u_j'}) = -\frac{1}{\rho} \frac{\partial p'}{\partial x_i} u_i' + \nu \frac{\partial^2 u_i' u_i'}{\partial x_j^2}$$

So, we will start from the Navier-Stokes equations and intentionally from and we will derive the equation for turbulent kinetic energy. So, you know that in general, we have the Navier-Stokes equation, $\frac{\partial u_i}{\partial t} + \frac{\partial}{\partial x_j} (u_i u_j) = -\frac{1}{\rho} \frac{\partial p}{\partial x_i} + \nu \frac{\partial^2 u_i}{\partial x_j^2}$. Let us say this is equation number 1.

Now, if you substitute $u_i = \bar{u}_i + u_i'$ and $u_j = \bar{u}_j + u_j'$ and $p = \bar{p} + p'$ ok. So, these are Reynolds decomposition.

So, if you substitute it here ok and if you take the average of the entire equation, then we will get $\frac{\partial \bar{u}_i}{\partial t} + \frac{\partial}{\partial x_j} (\bar{u}_i \bar{u}_j + \overline{u_i' u_j'}) = -\frac{1}{\rho} \frac{\partial \bar{p}}{\partial x_i} + \nu \frac{\partial^2 \bar{u}_i}{\partial x_j^2}$.

$\frac{\partial \bar{p}}{\partial x_i} - \frac{1}{\rho} \frac{\partial \bar{p}'}{\partial x_i} + \frac{\partial}{\partial x_j} \nu \frac{\partial \bar{u}_i}{\partial x_j} - \frac{\partial}{\partial x_j} \nu \frac{\partial \bar{u}_i'}{\partial x_j}$

So, you can see that some of the terms will be 0. So, because you know that the time average of this fluctuating component \bar{u}_i' will be 0. So, this will be 0 ok, you can see that this term ok. So, this will be 0, this term will be 0, this term will be 0 and you can see this is also the time average of this fluctuating component. So, this will be also 0 ok.

So, you can see that after substituting this here and taking the average, we just wrote this and after simplification we can write this equation as $\frac{\partial \bar{u}_i}{\partial t} + \frac{\partial}{\partial x_j} \bar{u}_i \bar{u}_j - \bar{u}_i' \bar{u}_j'$ is equal to $-\frac{1}{\rho} \frac{\partial \bar{p}}{\partial x_i} + \frac{\partial}{\partial x_j} \nu \frac{\partial \bar{u}_i}{\partial x_j} - \frac{\partial}{\partial x_j} \nu \frac{\partial \bar{u}_i'}{\partial x_j}$ ok.

And; obviously, this is the Reynolds state. So, that we can take in the left hand side and we can write $\frac{\partial \bar{u}_i}{\partial t} + \frac{\partial}{\partial x_j} \bar{u}_i \bar{u}_j$ is equal to $-\frac{1}{\rho} \frac{\partial \bar{p}}{\partial x_i} + \frac{\partial}{\partial x_j} \nu \frac{\partial \bar{u}_i}{\partial x_j} - \frac{\partial}{\partial x_j} \nu \frac{\partial \bar{u}_i'}{\partial x_j}$. So, we are taking this term in the right hand side which is your Reynolds stress bar, let us say that this is equation number 2.

So, now you subtract equation number 2 from equation number 1, then let us write the equation in terms of the velocity fluctuations. So, you can see that; obviously, if you subtract this equation 2 from equation 1, then you will get this $\bar{u}_i - \bar{u}_i'$ which we can represent in terms of this fluctuating velocity \bar{u}_i' . So, we can write subtracting, subtract equation 2 from equation 1 ok, then what we will get?

We can write $\frac{\partial \bar{u}_i'}{\partial t}$ because $\bar{u}_i - \bar{u}_i'$ sorry, $\bar{u}_i - \bar{u}_i'$ will be $\bar{u}_i' + \frac{\partial}{\partial x_j} \bar{u}_j$. It will be $\bar{u}_i' + \bar{u}_j' + \bar{u}_j \bar{u}_i' + \bar{u}_i' \bar{u}_j' - \bar{u}_i' \bar{u}_j'$. So, you make some additional simplification then you will get this.

Then right hand side we have $-\frac{1}{\rho} \frac{\partial \bar{p}'}{\partial x_i} + \frac{\partial}{\partial x_j} \nu \frac{\partial \bar{u}_i'}{\partial x_j}$ ok. So, this is equation number 3. Now, multiply equation 3 by \bar{u}_i' ok.

So, that we can write in terms of the turbulent kinetic energy, you can see that if you multiply u_i' here. So, it will be $u_i'^2$ and that is the representation of this turbulent kinetic energy.

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Turbulence Modelling

$$u_i' \frac{\partial u_i'}{\partial t} + u_i' \frac{\partial}{\partial x_j} (\bar{u}_i u_j') + u_i' \frac{\partial}{\partial x_j} (\bar{u}_j u_i') + u_i' \frac{\partial}{\partial x_j} (u_i' u_j') + u_i' \frac{\partial}{\partial x_j} (\overline{u_i' u_j'})$$

$$= -\frac{1}{\rho} u_i' \frac{\partial p'}{\partial x_i} + u_i' \frac{\partial}{\partial x_j} (\nu \frac{\partial u_i'}{\partial x_j})$$

Term 1: $\frac{\partial}{\partial t} (\frac{1}{2} u_i'^2)$

Term 2: $u_i' (\bar{u}_i \frac{\partial u_j'}{\partial x_j} + u_j' \frac{\partial \bar{u}_i}{\partial x_j}) = u_i' u_j' \frac{\partial \bar{u}_i}{\partial x_j}$

Term 3: $u_i' (\bar{u}_j \frac{\partial u_i'}{\partial x_j} + u_i' \frac{\partial \bar{u}_j}{\partial x_j}) = u_i' \bar{u}_j \frac{\partial u_i'}{\partial x_j} = \bar{u}_j \frac{\partial}{\partial x_j} (\frac{1}{2} u_i'^2)$

Term 4: $u_i' (u_i' \frac{\partial u_j'}{\partial x_j} + u_j' \frac{\partial u_i'}{\partial x_j}) = u_j' \frac{\partial}{\partial x_j} (\frac{1}{2} u_i'^2)$

$$= \frac{\partial}{\partial x_j} (u_j' \frac{1}{2} u_i'^2) - \frac{1}{2} u_i'^2 \frac{\partial u_j'}{\partial x_j}$$

$$= \frac{\partial}{\partial x_j} (u_j' \frac{1}{2} u_i'^2)$$

Term 5: $u_i' \frac{\partial}{\partial x_j} (\overline{u_i' u_j'})$

So, if you write that then you can see that we can write $u_i' \frac{\partial u_i'}{\partial t} + u_i' \frac{\partial}{\partial x_j} (\bar{u}_i u_j' + \bar{u}_j u_i' + u_i' u_j' - \overline{u_i' u_j'})$ is equal to $-\frac{1}{\rho} \frac{\partial p'}{\partial x_i} + \nu \frac{\partial^2 u_i'}{\partial x_j^2}$.

So, here you need to multiply with u_i' and if you multiply here by u_i' then we can write this term. So, now, each term let us individually see ok. So, if you write this equation as $u_i' \frac{\partial u_i'}{\partial t} + u_i' \frac{\partial}{\partial x_j} (\bar{u}_i u_j' + \bar{u}_j u_i' + u_i' u_j' - \overline{u_i' u_j'})$

$\frac{\partial}{\partial x_j} (u_i - u_j) = -\frac{1}{\rho} \frac{\partial p}{\partial x_i} + \nu \frac{\partial^2 u_i}{\partial x_j^2}$

So, now let us look each an individual these terms ok. So, let us say this is. So, this is your 1, this is term 2, this is 3, this is 4, this is 5, this is 6 and this is 7 ok. So, let us say term 1 ok. So, what we can write? So, if you take u_i inside. So, we can write this term as $\frac{\partial}{\partial t} \frac{1}{2} u_i^2$ ok. So, u_i if you take inside then; obviously, it will become half $\frac{\partial}{\partial t} u_i^2$.

Now, term 2. So, this term you can see that this we can write as $u_i \frac{\partial u_j}{\partial x_j} + u_j \frac{\partial u_i}{\partial x_j}$ ok and then we can write you can see that this is nothing but the continuity equation satisfying the fluctuating velocity component. So, this will be 0, right.

So, you can see that this term is 0 because this is actually the continuity equation satisfying by the velocity fluctuating components ok. So, that we have already derived. So, this will get as $u_j \frac{\partial u_i}{\partial x_j} + u_i \frac{\partial u_j}{\partial x_j}$ and we have another u_i . So, we can write this term as $u_i \frac{\partial u_j}{\partial x_j}$.

Now, term 3 ok. Similarly, we can write $u_i \frac{\partial u_j}{\partial x_j} + u_j \frac{\partial u_i}{\partial x_j}$ plus $u_i \frac{\partial u_j}{\partial x_j}$. So, here you can see that this is the continuity equation satisfied by the mean velocity. So, this will become 0 ok. So, this is 0. So, we will get $u_i \frac{\partial u_j}{\partial x_j}$. Now, you take this u_i again inside this derivative. So, what we will write $u_j \frac{\partial}{\partial x_j} \frac{1}{2} u_i^2$. Now, let us write this term 4. So, you can see this is the term 4.

So, similarly you can write $u_i \frac{\partial u_j}{\partial x_j} + u_j \frac{\partial u_i}{\partial x_j}$ plus $u_j \frac{\partial u_i}{\partial x_j}$. So, this is also 0, right. So, this is 0. So, we can write. So, this now we can write. So, $u_i \frac{\partial u_j}{\partial x_j}$ this. So, you can write $u_j \frac{\partial u_i}{\partial x_j}$ and $u_i \frac{\partial u_j}{\partial x_j}$ if you take inside. So, we can write $\frac{\partial}{\partial x_j} \frac{1}{2} u_i^2$ ok and now, if you take this u_j inside this derivative.

So, what we can write? We can write $\frac{\partial}{\partial x_j} u_j' \frac{1}{2} u_i'^2$ as we have taken inside. So, there will be minus $\frac{1}{2} u_i'^2 \frac{\partial}{\partial x_j} u_j'$ by $\frac{\partial}{\partial x_j} u_j'$ ok. So, you can see again this is 0 right ok. So, we can write this term as $\frac{\partial}{\partial x_j} u_j' \frac{1}{2} u_i'^2$. Now, let us consider this term 5 ok. So, term 5 if you write ok. So, we can see that we can, we will keep as it is ok $u_i' \frac{\partial}{\partial x_j} p'$ ok.

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Turbulence Modelling

Term 6: $\frac{u_i'}{\rho} \frac{\partial p'}{\partial x_i} = \frac{\partial}{\partial x_i} \left(\frac{1}{\rho} u_i' p' \right) - \frac{1}{\rho} p' \frac{\partial u_i'}{\partial x_i}$
 $= \frac{\partial}{\partial x_i} \left(\frac{1}{\rho} u_i' p' \right)$

Term 7: $u_i' \frac{\partial}{\partial x_j} \left(\nu \frac{\partial u_i'}{\partial x_j} \right)$
 $= \frac{\partial}{\partial x_j} \left(\nu u_i' \frac{\partial u_i'}{\partial x_j} \right) - \nu \frac{\partial u_i'}{\partial x_j} \frac{\partial u_i'}{\partial x_j}$

Now, part 6 and part 7. Now, let us simplify part 6 ok. So, we have this term $u_i' \frac{\partial}{\partial x_i} p'$ by $\frac{\partial}{\partial x_i} u_i'$. So, we will take u_i' inside. So, you can write this as $\frac{\partial}{\partial x_i} u_i' p'$, let us keep the viscosity also. So, we can write $\frac{1}{\rho} u_i' p'$ minus $\frac{1}{\rho} p' \frac{\partial u_i'}{\partial x_i}$ by $\frac{\partial}{\partial x_i} u_i'$ ok.

So, now this is again continuity equation. So, this will be 0. We can write this term as $\frac{\partial}{\partial x_i} \frac{1}{\rho} u_i' p'$. And the last term part 7, sorry you were writing term. So,

this is term 6 and term 7. So, you have $u_i' \frac{\partial}{\partial x_j} \nu \frac{\partial u_i'}{\partial x_j}$. So, if you take this inside. So, you can write $\frac{\partial}{\partial x_j} (\nu u_i' \frac{\partial u_i'}{\partial x_j})$ minus $\nu \frac{\partial}{\partial x_j} (\frac{\partial u_i'}{\partial x_j})$.

So, you can see that all the terms we have written in such a way that we can define the turbulent kinetic energy or you can represent the turbulent kinetic energy.

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Turbulence Modelling

$$\frac{\partial}{\partial t} (\frac{1}{2} u_i'^2) + u_i' u_j' \frac{\partial \bar{u}_i}{\partial x_j} + \bar{u}_j \frac{\partial}{\partial x_j} (\frac{1}{2} u_i'^2) + \frac{\partial}{\partial x_j} (u_j' \frac{1}{2} u_i'^2) + u_i' \frac{\partial}{\partial x_j} (-\bar{u}_i' u_j') = -\frac{\partial}{\partial x_i} (\frac{1}{\rho} u_i' p') + \frac{\partial}{\partial x_j} (2 u_i' \frac{\partial u_i'}{\partial x_j}) \rightarrow \frac{\partial u_i'}{\partial x_j} \frac{\partial u_i'}{\partial x_j}$$

Take the time average of the above eqn.

$$\frac{\partial}{\partial t} (\frac{1}{2} \overline{u_i'^2}) + \overline{u_i' u_j'} \frac{\partial \bar{u}_i}{\partial x_j} + \bar{u}_j \frac{\partial}{\partial x_j} (\frac{1}{2} \overline{u_i'^2}) + \frac{\partial}{\partial x_j} (\overline{u_j' \frac{1}{2} u_i'^2}) + \overline{u_i'} \frac{\partial}{\partial x_j} (-\overline{u_i' u_j'}) = -\frac{\partial}{\partial x_i} (\frac{1}{\rho} \overline{u_i' p'}) + \frac{\partial}{\partial x_j} (2 \overline{u_i' \frac{\partial u_i'}{\partial x_j}}) - 2 \frac{\partial \overline{u_i'} \frac{\partial u_i'}{\partial x_j}}{\partial x_j}$$

$$\frac{\partial k}{\partial t} + \bar{u}_j \frac{\partial k}{\partial x_j} = -\frac{\partial}{\partial x_j} (\frac{1}{2} \overline{u_j' u_i'^2} + \frac{1}{\rho} \overline{u_i' p'} - 2 \overline{u_i' \frac{\partial u_i'}{\partial x_j}}) - \overline{u_i' u_j'} \frac{\partial \bar{u}_i}{\partial x_j} - 2 \frac{\partial \overline{u_i' \frac{\partial u_i'}{\partial x_j}}}{\partial x_j}$$

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So, now all these terms, from term 1 to term 7, let us put in the original equation. So, if you put we will be get $\frac{\partial}{\partial t} \frac{1}{2} \overline{u_i'^2}$ plus $\overline{u_i' u_j'} \frac{\partial \bar{u}_i}{\partial x_j}$ plus $\bar{u}_j \frac{\partial}{\partial x_j} (\frac{1}{2} \overline{u_i'^2})$ plus $\frac{\partial}{\partial x_j} (\overline{u_j' \frac{1}{2} u_i'^2})$ plus $\overline{u_i'} \frac{\partial}{\partial x_j} (-\overline{u_i' u_j'})$ minus $\frac{\partial}{\partial x_i} (\frac{1}{\rho} \overline{u_i' p'})$ plus $\frac{\partial}{\partial x_j} (2 \overline{u_i' \frac{\partial u_i'}{\partial x_j}})$ minus $2 \frac{\partial \overline{u_i' \frac{\partial u_i'}{\partial x_j}}}{\partial x_j}$.

So, in the right hand side we have minus $\frac{\partial}{\partial x_i} (\rho u_i' p')$ plus $\frac{\partial}{\partial x_j} (\nu u_i' \frac{\partial u_i'}{\partial x_j})$ and minus $\nu \frac{\partial u_i'}{\partial x_j}$. So, next what we will do? We will take the time average of this whole equation ok. So, take the time average of the above equation ok. So, then we can represent as $\frac{\partial}{\partial t} \frac{1}{2} \overline{u_i'^2} + \overline{u_i' u_j'} \frac{\partial \overline{u_i'}}{\partial x_j} + \overline{u_j' \frac{\partial u_i'}{\partial x_j}}$ plus $\frac{\partial}{\partial x_j} \frac{1}{2} \overline{u_i'^2}$ plus $\frac{\partial}{\partial x_j} \nu \overline{u_i' \frac{\partial u_i'}{\partial x_j}}$.

So, we have this $\overline{u_j' u_i' \frac{\partial u_i'}{\partial x_j}}$ plus this will be $\overline{u_i' \frac{\partial u_i'}{\partial x_j}}$ minus $\overline{u_i' u_j' \frac{\partial u_i'}{\partial x_j}}$ and right hand side we have $\frac{\partial}{\partial x_i} (\rho u_i' p')$ plus $\frac{\partial}{\partial x_j} (\nu u_i' \frac{\partial u_i'}{\partial x_j})$ minus $\nu \frac{\partial u_i'}{\partial x_j}$. So, you can see that this we have already defined as dissipation rate per unit kinetic energy right.

So, this is the dissipation rate. So, now, we can see this is the representation of this turbulent kinetic energy and you can see that this is $\overline{u_i'^2}$. So, $\overline{u_i'}$ will be 0. So, this term is 0. So, now, we can write the equation ok. So, this we will write as $\frac{\partial}{\partial t}$. So, this we will write k because this is the turbulent kinetic energy $\frac{1}{2} \overline{u_i'^2}$ plus now this term you see, this term ok.

So, this we write as $\overline{u_j' \frac{\partial u_i'}{\partial x_j}}$ and this will be $\frac{\partial k}{\partial x_j}$ ok, this is the turbulent kinetic energy. In the right hand side if you take so these terms. So, we can write minus $\frac{\partial}{\partial x_j} (\rho u_i' p')$ ok what are the terms we have. So, this is one term, $\frac{1}{2} \overline{u_j' \frac{\partial u_i'}{\partial x_j}}$ plus $\frac{1}{\rho}$. So, this will be x_i ok.

So, now this x_i were interchanging with j . So, you can write $\frac{1}{\rho} \frac{\partial}{\partial x_j} (\rho u_i' p')$ we have written. So, $\overline{u_j' \frac{\partial u_i'}{\partial x_j}}$ you can write $\overline{p' u_j'}$ ok. Then we have minus $\nu \frac{\partial u_i'}{\partial x_j}$ this term, $\frac{\partial u_i'}{\partial x_j}$ ok. What are the additional terms we have? So, this is one term. So, this will be minus $\overline{u_i' u_j' \frac{\partial u_i'}{\partial x_j}}$ and another term we have this term.

So, it will be minus nu del u i prime by del x j del u i prime by del x j bar. So, this you can see this we have already defined as the dissipation rate epsilon ok.

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Turbulence Modelling

Standard $k - \epsilon$ model

$$\frac{\partial k}{\partial t} + \bar{u}_j \frac{\partial k}{\partial x_j} = -\frac{\partial}{\partial x_j} \left(\frac{1}{2} \overline{u'_j u'_j u'_j} + \frac{1}{\rho} \overline{u'_j p'} - \nu \overline{u'_j \frac{\partial u'_j}{\partial x_j}} \right) - \underbrace{\overline{u'_j \frac{\partial \bar{u}_i}{\partial x_j}}}_{P} - \underbrace{\nu \frac{\partial \overline{u'_j \frac{\partial u'_j}{\partial x_j}}}{\partial x_j}}_{\epsilon}$$

Turbulent kinetic energy:

$$\frac{Dk}{Dt} = \frac{\partial k}{\partial t} + \bar{u}_j \frac{\partial k}{\partial x_j} = \frac{\partial}{\partial x_j} \left[\frac{\nu_t}{\sigma_k} \frac{\partial k}{\partial x_j} \right] + P - \epsilon$$

↑ Rate of change of k ↑ Convective term ↑ Diffusive term ↑ Rate of production ← Rate of destruction.

Dissipation rate of k :

$$\frac{D\epsilon}{Dt} = \frac{\partial \epsilon}{\partial t} + \bar{u}_j \frac{\partial \epsilon}{\partial x_j} = \frac{\partial}{\partial x_j} \left[\frac{\nu_t}{\sigma_\epsilon} \frac{\partial \epsilon}{\partial x_j} \right] + C_{\epsilon 1} \frac{P\epsilon}{k} - C_{\epsilon 2} \frac{\epsilon^2}{k}$$

So, now, you can see that we have derived the equation for this turbulent kinetic energy k ok. So, let us see the significance of each terms. So, you can see this is the equation we have already derived ok and this term we can write as the production term ok. This term as we can write as production term P and this is the dissipation rate epsilon ok and you can see that these terms we can model because these fluctuating velocity components are unknown. So, that we can write del of del x j nu t by sigma k del k by del x j.

So, these are some model constant sigma k and; obviously, nu t is the turbulent viscosity. And this is the term P we are representing and this is the dissipation rate epsilon. So, you can see that this is a convective diffusive equation right. So, you can see this left hand side is the

inertia term, this we can represent as a viscous term and some additional such terms are there ok.

So, you can see that it is a rate of change of k ok. So, this term is rate of change of k ok. So, k is the turbulent kinetic energy and this is the; obviously, you can see that inertia term ok. So, convective term and this you can see that this is diffusive term and this term ok we are representing as P which is your rate of production and this ϵ is your dissipation. So, it is rate of destruction.

So, you can see that to solve this equation, we need to know the value of ν_t as well as the dissipation rate ϵ . So, we need another equation for dissipation rate ϵ . So, we are not going into detail of derivation of this equation, but we are writing the final equation for the dissipation rate. So, you can see dissipation rate of k is this after using some model constants and these model constants are found by picking the data from the experimental values ok.

So, you can see again this is the similar way, this is rate of change of ϵ , this is the convective term, this is the diffusive term and this is the rate of production and this is the rate of destruction ok. So, now, we need to know all these model constants, σ_k , σ_ϵ , $C_\epsilon 1$, $C_\epsilon 2$ and this P is the rate of production.

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Turbulence Modelling

Standard $k-\epsilon$ model

Model constants

$$C_\mu = 0.09, C_{\epsilon 1} = 1.44, C_{\epsilon 2} = 1.92, \sigma_k = 1, \sigma_\epsilon = 1.3$$

Eddy viscosity

$$\mu_t = \rho C_\mu \frac{k^2}{\epsilon}$$

So, you can see that in standard k epsilon model, there are some model constants which are found from the experiments. So, these are empirical constants. So, you can see C mu is 0.09, C epsilon 1 is 1.44, C epsilon 2 1.92, sigma k is 1 and sigma epsilon is 1.3. Once you find the value of k and the epsilon, then you will be able to calculate the eddy viscosity mu t as rho C mu k square by epsilon, where C mu is this model constant.

So, you can see that this k epsilon model has some advantages as it is relatively simple to implement and it is widely validated turbulence model. However, it has some disadvantages like it gives poor prediction for swirling and rotating flows and flows with strong separation.

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Turbulence Modelling

RNG $k - \epsilon$ model

$$\frac{\partial k}{\partial t} + u_j \frac{\partial k}{\partial x_j} = \nu_t \left(\frac{\partial \bar{u}_i}{\partial x_j} + \frac{\partial \bar{u}_j}{\partial x_i} \right) \frac{\partial \bar{u}_i}{\partial x_j} + \frac{\partial}{\partial x_i} \left(\alpha_k \left(\nu + C_\mu \frac{k^2}{\epsilon} \right) \frac{\partial k}{\partial x_i} \right) - \epsilon$$

$$\frac{\partial \epsilon}{\partial t} + u_j \frac{\partial \epsilon}{\partial x_j} = C_{1\epsilon} \frac{\epsilon}{k} \nu_t \left(\frac{\partial \bar{u}_i}{\partial x_j} + \frac{\partial \bar{u}_j}{\partial x_i} \right) \frac{\partial \bar{u}_i}{\partial x_j} + \frac{\partial}{\partial x_i} \left(\alpha_\epsilon \left(\nu + C_\mu \frac{k^2}{\epsilon} \right) \frac{\partial \epsilon}{\partial x_i} \right) - C_{2\epsilon} \frac{\epsilon^2}{k} - R$$

Model constants

$$C_\mu = 0.0845, C_{1\epsilon} = 1.42, C_{2\epsilon} = 1.68, \alpha_k = 1.39, \alpha_\epsilon = 1.68$$

Eddy viscosity $\mu_t = \rho C_\mu \frac{k^2}{\epsilon}$

So, there are some improved models like RNG k epsilon model. RNG stands for renormalization group model and here we solve two equations, one for k and another equation is epsilon with some different empirical constants and you can see these are the model constants. So, C mu is 0.0845, C 1 epsilon is 1.42, C 2 epsilon is 1.68, alpha k is 1.39 and alpha epsilon is 1.68.

So; obviously, these equations you can see here these model constants are there and these you need to use these model constants and once you find this k and epsilon you will be able to calculate this eddy viscosity mu t as rho C mu k square by epsilon. So, obviously, you can see that it has impute prediction for flows with high steam line curvature and strain rate and transitional flows.

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Turbulence Modelling

k - ω model

Dissipation per unit kinetic energy, ω

$$\frac{\partial k}{\partial t} + u_j \frac{\partial k}{\partial x_j} = \frac{\partial}{\partial x_j} \left[\nu + \frac{\nu_t}{\sigma_k} \frac{\partial k}{\partial x_j} \right] + \nu_t \left(\frac{\partial \bar{u}_i}{\partial x_j} + \frac{\partial \bar{u}_j}{\partial x_i} \right) \frac{\partial \bar{u}_i}{\partial x_j} - \beta^* k \omega$$

$$\frac{\partial \omega}{\partial t} + u_j \frac{\partial \omega}{\partial x_j} = \frac{\partial}{\partial x_j} \left[\nu + \frac{\nu_t}{\sigma_\omega} \frac{\partial \omega}{\partial x_j} \right] + \alpha \nu_t \left(\frac{\partial \bar{u}_i}{\partial x_j} + \frac{\partial \bar{u}_j}{\partial x_i} \right) \frac{\partial \bar{u}_i}{\partial x_j} - \beta_1 \omega^2$$

Model constants

$$\beta_1 = 0.075, \beta^* = 0.09, \alpha = 0.553, \sigma_k = 2.0, \sigma_\omega = 2.0$$

Eddy viscosity $\mu_t = \rho \frac{k}{\omega}$

Another two equation model is there, that is known as k omega model, where omega is the dissipation per unit kinetic energy. So, we are not going into details of derivation of these equations, but we are writing this equation. So, this is the equation for k and this is the equation for this dissipation per unit kinetic energy omega.

So, here you can see that there are some model constants like here you have sigma k, beta star, alpha, beta 1. So, these are the empirical constants beta 1 is equal to 0.075, beta star is equal to 0.09, alpha is equal to 0.553, sigma k is equal to 2, sigma omega is equal to 2. So, once we solve these two equations, then we will be able to find k and omega and from there we can find the eddy viscosity mu t as rho k by omega.

So, this k omega model has much application in aerospace engineering. It gives improve performance for boundary layers under adverse pressure gradient. So, there are different

turbulence model, we have discussed where standard k epsilon model is a versatile model where you have the flow separation and it is best for industrial internal flows and also this model is good for this aerospace application.

However, we have this RNG k epsilon model which is good for transitional flow and for this k omega where you have rotational flow we have much strain rate. So, in those cases we can actually use this k omega model.

Thank you.